

On a diphasic low Mach model for a heat exchanger

Theoretical and 1D/2D numerical results

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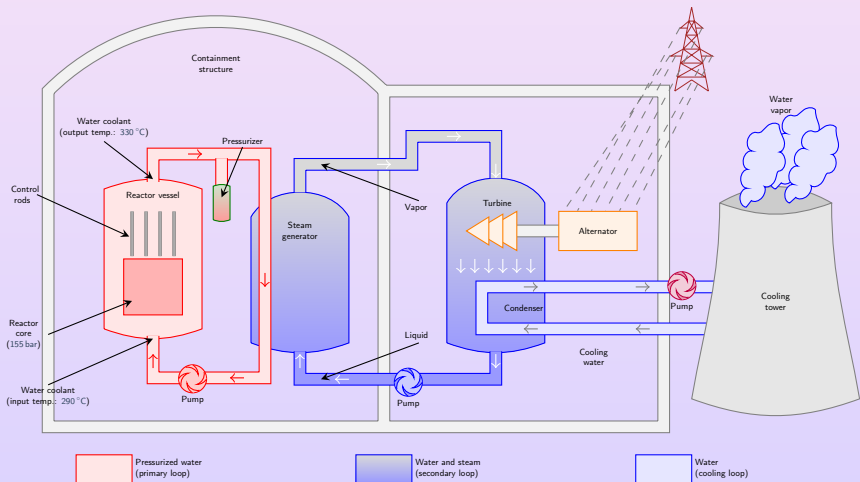
Outline

- 1 Context
- 2 The Low Mach Hypothesis
- 3 A Low Mach model for a heat exchanger
- 4 Theoretical results: 1D-model
- 5 Numerical schemes
- 6 Conclusion & Perspectives

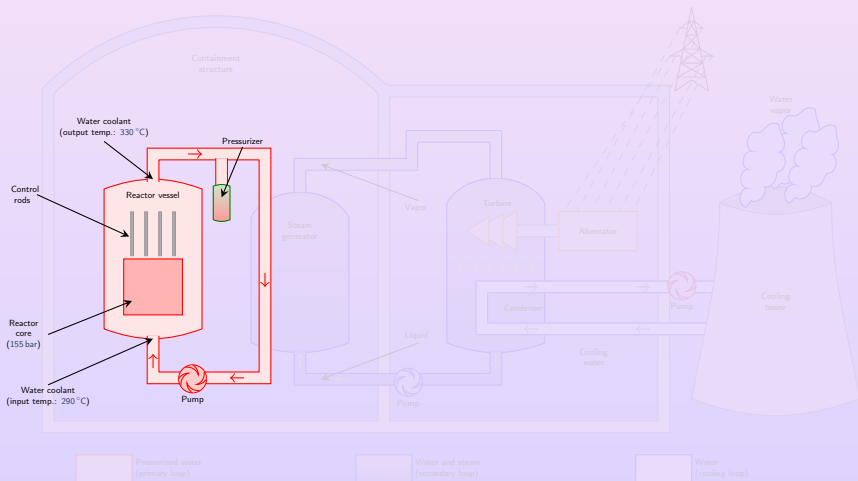
Section 1

Context

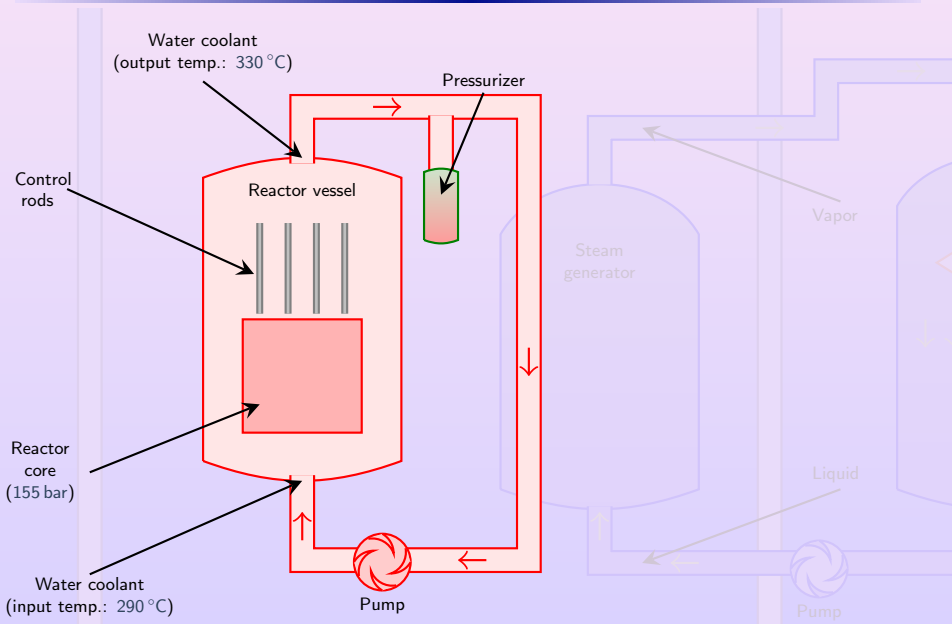
Pressurized Water Reactor



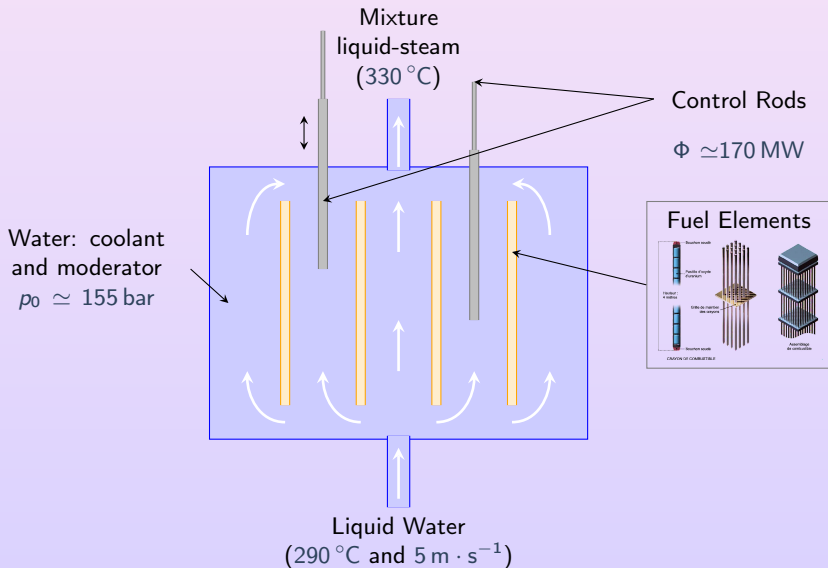
Pressurized Water Reactor



Pressurized Water Reactor



Core of a Pressurized Water Reactor



Section 2

The Low Mach Hypothesis

Core at Pressurized Water Reactor

Nominal regime

- Inlet velocity: $|\mathbf{u}| \simeq 5 \text{ m} \cdot \text{s}^{-1}$
- Speed of sound at $p_0 = 155 \text{ bar}$ and $T = 300 \text{ }^\circ\text{C}$: $c_\ell^* \simeq 1.0 \times 10^3 \text{ m} \cdot \text{s}^{-1}$

$$\text{Mach number } M = \frac{|\mathbf{u}|}{c_\ell^*} \simeq 5 \times 10^{-3} \ll 1$$

This is also the case

- for incidental regime
- for some accidental scenarios such as a LOFA (Loss of Flow Accident)¹ induced by a coolant pump trip event *even if phase change occurs*

Acoustics negligible (no shock waves) BUT high heat transfers

¹Except for a very fast depressurization such as a LOCA (Loss of Coolant Accident)

Core at Pressurized Water Reactor

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Which model?

- Low Mach number: $M \ll 1$
- High heat transfers: $\operatorname{div} \mathbf{u} \neq 0$



- 1 Compressible Navier-Stokes system
→ model with acoustics and with heat transfers
- 2 Asymptotic low Mach model
(obtained formally by filtering out the acoustics waves)
→ model without acoustics but with heat transfers

Section 3

A Low Mach model for a heat exchanger

- Governing equations
- Boundary Conditions
- Equation(s) of State

Section 3

A Low Mach model for a heat exchanger

- Governing equations
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An Asymptotic Low Mach Model

$$p(t, \mathbf{x}) = p_0(t) + \bar{p}(t, \mathbf{x}) \text{ with } \frac{\bar{p}(t, \mathbf{x})}{p_0(t)} = \mathcal{O}(M^2)$$

$$\begin{cases} \operatorname{div}(\mathbf{u}) = -\frac{p_0'(t)}{\varrho(h, p_0)(c^*(h, p_0))^2} + \frac{\beta(h, p_0)}{p_0(t)} [\Phi + \operatorname{div}(\lambda \cdot \nabla T(h, p_0))] \\ \varrho(h, p_0) (\partial_t h + \mathbf{u} \cdot \nabla h) = \Phi + p_0'(t) + \operatorname{div}(\lambda \cdot \nabla T(h, p_0)) \\ \varrho(h, p_0) (\partial_t \mathbf{u} + (\mathbf{u} \cdot \nabla) \mathbf{u}) + \nabla \bar{p} = \operatorname{div}(\sigma(\mathbf{u})) + \varrho(h, p_0) \mathbf{g} \end{cases}$$

- ▶ **Unknowns**
- ▶ **Given quantities**
- ▶ **Equation Of State:**

An Asymptotic Low Mach Model

$$p(t, \mathbf{x}) = p_0(t) + \bar{p}(t, \mathbf{x}) \text{ with } \frac{\bar{p}(t, \mathbf{x})}{p_0(t)} = \mathcal{O}(M^2)$$

$$\begin{cases} \operatorname{div}(\mathbf{u}) = -\frac{p_0'(t)}{\varrho(h, p_0)(c^*(h, p_0))^2} + \frac{\beta(h, p_0)}{p_0(t)} [\Phi + \operatorname{div}(\lambda \cdot \nabla T(h, p_0))] \\ \varrho(h, p_0) (\partial_t h + \mathbf{u} \cdot \nabla h) = \Phi + p_0'(t) + \operatorname{div}(\lambda \cdot \nabla T(h, p_0)) \\ \varrho(h, p_0) (\partial_t \mathbf{u} + (\mathbf{u} \cdot \nabla) \mathbf{u}) + \nabla \bar{p} = \operatorname{div}(\sigma(\mathbf{u})) + \varrho(h, p_0) \mathbf{g} \end{cases}$$

▼ Unknowns

- $(t, \mathbf{x}) \mapsto \mathbf{u}$ velocity
- $(t, \mathbf{x}) \mapsto h$ enthalpy
- $(t, \mathbf{x}) \mapsto \bar{p}$ dynamic pressure

▶ Given quantities

▶ Equation Of State:

An Asymptotic Low Mach Model

$$p(t, \mathbf{x}) = p_0(t) + \bar{p}(t, \mathbf{x}) \text{ with } \frac{\bar{p}(t, \mathbf{x})}{p_0(t)} = \mathcal{O}(M^2)$$

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► Unknowns

▼ Given quantities

- $(t, \mathbf{x}) \mapsto \Phi \geq 0$ power density
- \mathbf{g} gravity
- $t \mapsto p_0$ thermodynamic pressure

► Equation Of State:

An Asymptotic Low Mach Model

$$p(t, \mathbf{x}) = p_0(t) + \bar{p}(t, \mathbf{x}) \text{ with } \frac{\bar{p}(t, \mathbf{x})}{p_0(t)} = \mathcal{O}(M^2)$$

$$\begin{cases} \operatorname{div}(\mathbf{u}) = -\frac{p_0'(t)}{\varrho(h, p_0)(c^*(h, p_0))^2} + \frac{\beta(h, p_0)}{p_0(t)} [\Phi + \operatorname{div}(\lambda \cdot \nabla T(h, p_0))] \\ \varrho(h, p_0) (\partial_t h + \mathbf{u} \cdot \nabla h) = \Phi + p_0'(t) + \operatorname{div}(\lambda \cdot \nabla T(h, p_0)) \\ \varrho(h, p_0) (\partial_t \mathbf{u} + (\mathbf{u} \cdot \nabla) \mathbf{u}) + \nabla \bar{p} = \operatorname{div}(\sigma(\mathbf{u})) + \varrho(h, p_0) \mathbf{g} \end{cases}$$

► **Unknowns**

► **Given quantities**

▼ **Equation Of State:** $(h, p_0) \mapsto \varrho$ density

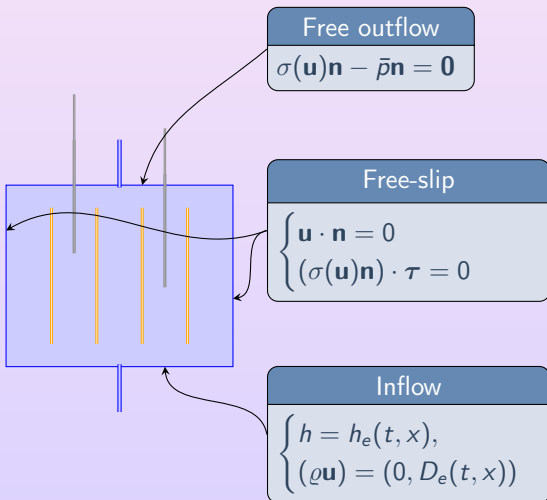
$$\Rightarrow \begin{cases} (h, p_0) \mapsto \beta \stackrel{\text{def}}{=} -\frac{p_0}{\varrho^2(h, p_0)} \left. \frac{\partial \varrho}{\partial h} \right|_{p_0} & \text{compressibility coefficient} \\ (h, p_0) \mapsto T & \text{temperature} \\ (h, p_0) \mapsto c^* & \text{speed of sound} \end{cases}$$

Section 3

A Low Mach model for a heat exchanger

- Governing equations
- **Boundary Conditions**
- Equation(s) of State

Boundary conditions



Section 3

A Low Mach model for a heat exchanger

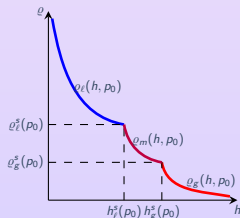
- Governing equations
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Diphasic EOS

- Liquid $\kappa = \ell$ and vapour $\kappa = g$ are characterized by their thermodynamic properties: $(h, p_0) \mapsto \varrho_\kappa$
- In the mixture, full equilibrium between liquid and vapour phases:
 $T = T^s(p_0)$ and we define values at saturation:

$$h_\kappa^s(p_0) \stackrel{\text{def}}{=} h_\kappa(p_0, T^s(p_0)), \quad \varrho_\kappa^s(p_0) \stackrel{\text{def}}{=} \varrho_\kappa(p_0, T^s(p_0)) = \varrho_\kappa(h_\kappa^s, p_0).$$

$$\varrho(h, p_0) = \begin{cases} \varrho_\ell(h, p_0), & \text{if } h \leq h_\ell^s(p_0), \\ \varrho_m(h, p_0) & \text{if } h_\ell^s(p_0) < h < h_g^s(p_0), \\ \varrho_g(h, p_0), & \text{if } h \geq h_g^s(p_0), \end{cases}$$



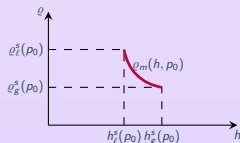
Mixture EoS

$$\begin{cases} \varrho = \alpha \varrho_g^s(p_0) + (1 - \alpha) \varrho_\ell^s(p_0) \\ \varrho h = \alpha \varrho_g^s(p_0) h_g^s(p_0) + (1 - \alpha) \varrho_\ell^s(p_0) h_\ell^s(p_0) \end{cases}$$

$$\text{for } h \in [h_\ell^s(p_0); h_g^s(p_0)]$$

$$\Downarrow$$

$$\varrho_m(h, p_0) = \frac{p_0 / \beta_m(p_0)}{h - q_m(p_0)}$$



where

$$\beta_m(p_0) \stackrel{\text{def}}{=} p_0 \frac{\frac{1}{\varrho_g^s} - \frac{1}{\varrho_\ell^s}}{h_g^s - h_\ell^s} = - \frac{p_0}{\varrho_m(h, p_0)} \left. \frac{\partial \varrho_m}{\partial h} \right|_{p_0} \quad q_m(p_0) \stackrel{\text{def}}{=} \frac{\varrho_g^s h_g^s - \varrho_\ell^s h_\ell^s}{\varrho_g^s - \varrho_\ell^s}$$

Pure phase EoS: Noble Able Stiffened Gas law

$$\frac{1}{\varrho_{\kappa}}(h, p_0) = \frac{\gamma_{\kappa} - 1}{\gamma_{\kappa}} \frac{h - q_{\kappa}}{p_0 + \pi_{\kappa}} + b_{\kappa}$$

- $\gamma_{\kappa} > 1$ adiabatic coefficient
- π_{κ} reference pressure
- q_{κ} binding energy
- b_{κ} covolume



$$\beta_{\kappa}(p_0) = - \frac{p_0}{\varrho_{\kappa}^2(h, p_0)} \left. \frac{\partial \varrho}{\partial h} \right|_{p_0} = \frac{\gamma_{\kappa} - 1}{\gamma_{\kappa}} \frac{p_0}{p_0 + \pi_{\kappa}} \quad \text{independent on } h$$



$$\varrho_{\kappa}(h, p_0) = \frac{p_0 / \beta_{\kappa}(p_0)}{h - \hat{q}_{\kappa}(p_0)}, \quad \hat{q}_{\kappa}(p_0) \stackrel{\text{def}}{=} q_{\kappa} - \frac{p_0}{\beta_{\kappa}(p_0)} b_{\kappa}$$

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⇓

$$\beta_\kappa(p_0) = -\frac{p_0}{\varrho_\kappa^2(h, p_0)} \left. \frac{\partial \varrho}{\partial h} \right|_{p_0} = \frac{\gamma_\kappa - 1}{\gamma_\kappa} \frac{p_0}{p_0 + \pi_\kappa} \quad \text{independent on } h$$

⇓

$$\varrho_\kappa(h, p_0) = \frac{p_0 / \beta_\kappa(p_0)}{h - \hat{q}_\kappa(p_0)}, \quad \hat{q}_\kappa(p_0) \stackrel{\text{def}}{=} q_\kappa - \frac{p_0}{\beta_\kappa(p_0)} b_\kappa$$

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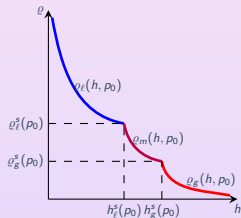
Diphasic Noble Able Stiffened Gas EOS

$$\varrho(h, p_0) = \frac{p_0 / \beta(h, p_0)}{h - \hat{q}(h, p_0)}$$

where

$$\hat{q}_\kappa(p_0) \stackrel{\text{def}}{=} q_\kappa - \frac{p_0}{\beta_\kappa(p_0)} b_\kappa$$

$$[\beta, q, b](h, p_0) = \begin{cases} [\beta, q, b]_\ell, & \text{if } h \leq h_\ell^s(p_0), \\ [\beta, q, 0]_m & \text{if } h_\ell^s(p_0) < h < h_g^s(p_0), \\ [\beta, q, b]_g, & \text{if } h \geq h_g^s(p_0), \end{cases}$$



Section 4

Theoretical results: 1D-model

- Steady state solution
- Analytical solutions with NASG

The LMNC model

$$p_0(t) = 155 \text{ bar } \forall t$$

$$\lambda = 0 \text{ W} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$$

1D

$$\begin{cases} \partial_y v = \frac{\beta(h)}{p_0} \Phi \\ \partial_t h + v \partial_y h = \frac{\Phi}{\rho(h)} \\ \partial_t (\rho(h)v) + \partial_y (\rho v^2 + \bar{p}) - \partial_y (\mu \partial_y v) = -g \rho(h) \end{cases}$$

Section 4

Theoretical results: 1D-model

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Steady state solution

$$(h_e^\infty, D_e^\infty > 0, \Phi^\infty(y)) \stackrel{\text{def}}{=} \lim_{t \rightarrow +\infty} (h_e(t), D_e(t), \Phi(t, y))$$

1 Enthalpy

Using $\partial_y(\varrho^\infty v^\infty) = 0$ we have $\partial_y h^\infty = \frac{\Phi^\infty}{D_e^\infty}$.

$$h^\infty(y) = h_e^\infty + \frac{\Psi(y)}{D_e^\infty}, \quad \Psi(y) \stackrel{\text{def}}{=} \int_0^y \Phi^\infty(z) dz$$

2 Velocity

$$v^\infty(y) = \frac{D_e^\infty}{\varrho(h^\infty(y))}$$

3 Dynamic pressure

Direct integration of $\partial_y \bar{p} = \partial_y(\mu \partial_y v) - \partial_y(\varrho v^2) - \varrho g$.

Section 4

Theoretical results: 1D-model

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Single phase

- ▶ **Velocity**
- ▶ **Enthalpy**

Single phase

▼ Velocity

Direct integration of $\partial_y v = \frac{\bar{\beta}}{\rho_0} \Phi$.

$$v(t, y) = v_e(t) + \frac{\bar{\beta}}{\rho_0} \Psi(t, y), \quad \Psi(t, y) \stackrel{\text{def}}{=} \int_0^y \Phi(t, z) \, dz$$

► Enthalpy

Single phase

► **Velocity**

▼ **Enthalpy**

Method of characteristics on $\partial_t h + v \partial_y h = \frac{\Phi}{\varrho(h)} = \Phi \left[\frac{\bar{\beta}}{p_0} (h - \hat{q}) \right]$.

Single phase

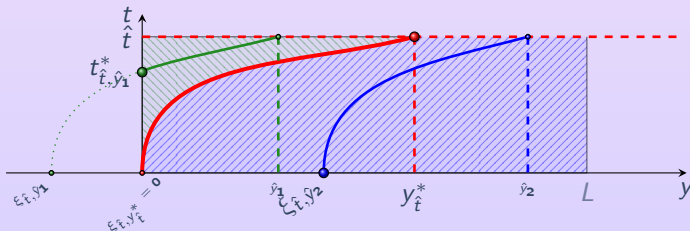
► Velocity

▼ Enthalpy

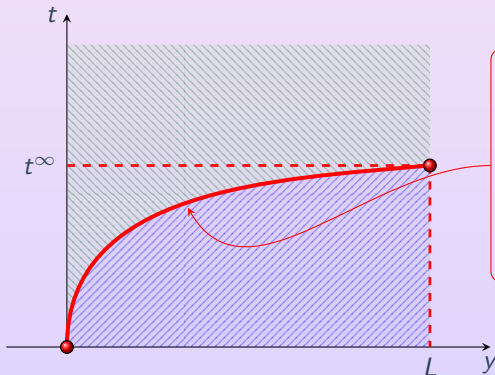
Method of characteristics on $\partial_t h + v \partial_y h = \frac{\Phi}{\rho(h)} = \Phi \left[\frac{\bar{\beta}}{\rho_0} (h - \hat{q}) \right]$.

Example: if Φ and v_e are constant, let $\hat{\Phi} \stackrel{\text{def}}{=} \frac{\bar{\beta} \Phi}{\rho_0}$ then

$$h(t, y) = \begin{cases} \hat{q} + (h_{\text{init}}(\xi_{t,y}) - \hat{q}) e^{\hat{\Phi} t} & \text{if } \xi_{t,y} \geq 0, \\ h_e(t_{t,y}^*) + \frac{\Phi}{D_e(t_{t,y}^*)} y & \text{if } \xi_{t,y} < 0. \end{cases}$$



Single phase



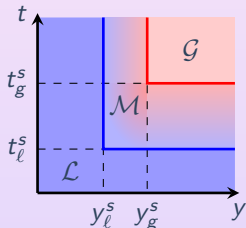
Characteristic $t = t(y)$:

$$y = \chi_{t^\infty, L}(t) = y_t^*$$

$$\Rightarrow \begin{cases} \xi_{t^\infty, L} = 0 \\ t_{t^\infty, L}^* = 0 \\ y_{t^\infty}^* = L \\ y_0^* = 0 \end{cases}$$

NASG two phases with phase transition

Φ , v_e , h_e , h_0 : constant; IC and BC: liquid phase.



$$y_\ell^s = \frac{D_e}{\Phi} (h_\ell^s - h_e)$$

$$y_g^s = \frac{D_e}{\Phi} (h_g^s - h_e)$$

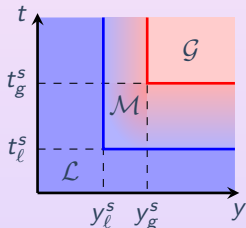
$$t_\ell^s = \frac{1}{\hat{\Phi}_\ell} \ln \left(\frac{h_\ell^s - \hat{q}_\ell}{h_0 - \hat{q}_\ell} \right)$$

$$t_g^s = t_\ell^s + \frac{1}{\hat{\Phi}_m} \ln \left(\frac{h_g^s - \hat{q}_m}{h_\ell^s - \hat{q}_m} \right)$$

- ▶ Velocity
- ▶ Enthalpy

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$$y_\ell^s = \frac{D_e}{\Phi} (h_\ell^s - h_e)$$

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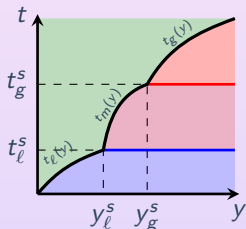
▼ **Velocity:** direct integration of $\partial_y v = \frac{\beta(h)}{\rho_0} \Phi$.

$$v(t, y) = \begin{cases} v_e + y \hat{\Phi}_\ell & \text{if } (t, y) \in \mathcal{L}, \\ v_e + y_\ell^s \hat{\Phi}_\ell + (y - y_\ell^s) \hat{\Phi}_m & \text{if } (t, y) \in \mathcal{M}, \\ v_e + y_\ell^s \hat{\Phi}_\ell + (y_g^s - y_\ell^s) \hat{\Phi}_m + (y - y_g^s) \hat{\Phi}_g & \text{if } (t, y) \in \mathcal{G}, \end{cases}$$

► Enthalpy

NASG two phases with phase transition

Φ , v_e , h_e , h_0 : constant; IC and BC: liquid phase.



$$y_\ell^s = \frac{D_e}{\Phi} (h_\ell^s - h_e)$$

$$y_g^s = \frac{D_e}{\Phi} (h_g^s - h_e)$$

$$t_\ell^s = \frac{1}{\hat{\Phi}_\ell} \ln \left(\frac{h_\ell^s - \hat{q}_\ell}{h_0 - \hat{q}_\ell} \right)$$

$$t_g^s = t_\ell^s + \frac{1}{\hat{\Phi}_m} \ln \left(\frac{h_g^s - \hat{q}_m}{h_\ell^s - \hat{q}_m} \right)$$

► Velocity

▼ **Enthalpy**: method of characteristics on $\partial_t h + v \partial_y h = \frac{\beta(h)\Phi}{\rho_0} (h - \hat{q}(h))$.

$$h(t, y) = \begin{cases} q_\ell + (h_0 - \hat{q}_\ell) e^{\hat{\Phi}_\ell t} & \text{if } (t, y) \in \mathcal{L} \text{ and } t < t_\ell(y), \\ q_m + (h_\ell^s - \hat{q}_m) e^{\hat{\Phi}_m(t-t_\ell^s)} & \text{if } (t, y) \in \mathcal{M} \text{ and } t < t_m(y), \\ q_g + (h_g^s - \hat{q}_g) e^{\hat{\Phi}_g(t-t_g^s)} & \text{if } (t, y) \in \mathcal{G} \text{ and } t < t_g(y), \\ h_e + \frac{\Phi}{D_e} y & \text{otherwise.} \end{cases}$$

Section 5

Numerical schemes

- 1D Numerical schemes
- 2D Numerical scheme

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Numerical schemes

- 1D Numerical schemes
- 2D Numerical scheme

MOC-scheme

- ▶ **Enthalpy**
- ▶ **Velocity**

MOC-scheme

▼ Enthalpy - key idea:

$$\partial_t h(t^{n+1}, y_i) + v(t^{n+1}, y_i) \partial_y h(t^{n+1}, y_i) = \frac{\Phi(t^{n+1}, y_i)}{\varrho(h(t^{n+1}, y_i))}$$

$$\Downarrow$$

$$\frac{d}{d\tau} \tilde{h}_i^{n+1}(\tau) = \frac{\Phi(\tau, \chi(\tau; t^{n+1}, y_i))}{\varrho(\tilde{h}_i^{n+1}(\tau))}$$

where $\bar{t} \in [t^n; t^{n+1}[$, $\tau \mapsto \tilde{h}_i^{n+1}(\tau) \stackrel{\text{def}}{=} h(\tau, \chi(\tau; t^{n+1}, y_i))$ and χ is the characteristic flow defined as the solution of

$$\begin{cases} \frac{d}{d\tau} \chi(\tau; t^{n+1}, y_i) = v(\tau, \chi(\tau; t^{n+1}, y_i)), & \tau \leq t^{n+1}, \\ \chi(t^{n+1}; t^{n+1}, y_i) = y_i. \end{cases}$$

► Velocity

MOC-scheme

▼ Enthalpy - key idea:

$$\partial_t h(t^{n+1}, y_i) + v(t^{n+1}, y_i) \partial_y h(t^{n+1}, y_i) = \frac{\Phi(t^{n+1}, y_i)}{\rho(h(t^{n+1}, y_i))}$$

↯

$$\int_{\bar{t}}^{t^{n+1}} \frac{d}{d\tau} \tilde{h}_i^{n+1}(\tau) d\tau = \int_{\bar{t}}^{t^{n+1}} \frac{\Phi(\tau, \chi(\tau; t^{n+1}, y_i))}{\rho(\tilde{h}_i^{n+1}(\tau))} d\tau$$

where $\bar{t} \in [t^n; t^{n+1}[$, $\tau \mapsto \tilde{h}_i^{n+1}(\tau) \stackrel{\text{def}}{=} h(\tau, \chi(\tau; t^{n+1}, y_i))$ and χ is the characteristic flow defined as the solution of

$$\begin{cases} \frac{d}{d\tau} \chi(\tau; t^{n+1}, y_i) = v(\tau, \chi(\tau; t^{n+1}, y_i)), & \tau \leq t^{n+1}, \\ \chi(t^{n+1}; t^{n+1}, y_i) = y_i. \end{cases}$$

► Velocity

MOC-scheme

▼ Enthalpy - key idea:

$$\partial_t h(t^{n+1}, y_i) + v(t^{n+1}, y_i) \partial_y h(t^{n+1}, y_i) = \frac{\Phi(t^{n+1}, y_i)}{\rho(h(t^{n+1}, y_i))}$$

⋮

$$h(t^{n+1}, y_i) - \tilde{h}_i^{n+1}(\bar{t}) = \int_{\bar{t}}^{t^{n+1}} \frac{d}{d\tau} \tilde{h}_i^{n+1}(\tau) d\tau = \int_{\bar{t}}^{t^{n+1}} \frac{\Phi(\tau, \chi(\tau; t^{n+1}, y_i))}{\rho(\tilde{h}_i^{n+1}(\tau))} d\tau$$

where $\bar{t} \in [t^n; t^{n+1}[$, $\tau \mapsto \tilde{h}_i^{n+1}(\tau) \stackrel{\text{def}}{=} h(\tau, \chi(\tau; t^{n+1}, y_i))$ and χ is the characteristic flow defined as the solution of

$$\begin{cases} \frac{d}{d\tau} \chi(\tau; t^{n+1}, y_i) = v(\tau, \chi(\tau; t^{n+1}, y_i)), & \tau \leq t^{n+1}, \\ \chi(t^{n+1}; t^{n+1}, y_i) = y_i. \end{cases}$$

► Velocity

MOC-scheme

▼ **Enthalpy** - scheme: let $\xi_i^n \approx \chi(t^n; t^{n+1}, y_i)$.

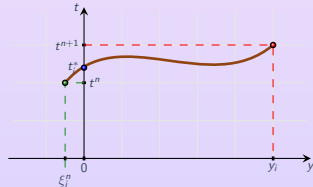
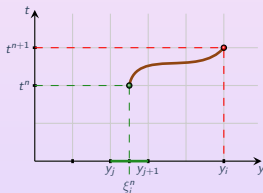
- If $\xi_i^n > 0$, let $\hat{h}_i^n \approx \tilde{h}_i^{n+1}(t^n)$ (at order 1 or higher) and then $\bar{t} = t^n$ and

$$h_i^{n+1} = \hat{h}_i^n + \Delta t \frac{\Phi(t^n, \xi_i^n)}{\varrho(\hat{h}_i^n)}$$

- If $\xi_i^n \leq 0$, let $t_i^* = t^{n+1} - y_i/v_i^n \approx \tau$ such that $\chi(\tau; t^{n+1}, y_i) = 0$ and then $\bar{t} = t_i^*$ and

$$h_i^{n+1} = h_e(t_i^*) + (t^{n+1} - t_i^*) \frac{\Phi(t_i^*, 0)}{\varrho(h_e(t_i^*))}$$

► **Velocity**



MOC-scheme

► Enthalpy

▼ Velocity : $\partial_y v = \frac{\beta(h)\Phi}{\rho_0}$

$$v_i^{n+1} = v_{i-1}^{n+1} + \frac{1}{\rho_0} \int_{y_{i-1}}^{y_i} \beta(h(t^{n+1}, z)) \Phi(t^{n+1}, z) dz$$

$$\approx v_{i-1}^{n+1} + \frac{\Delta y}{\rho_0} \beta(h_{i-1}^{n+1}) \Phi(t^{n+1}, y_{i-1}).$$

β is discontinuous at phase change points, so that if $h_{\kappa}^s \in (h_{i-1}^{n+1}, h_i^{n+1})$, let $y^* = y_{i-1} + \Delta y \frac{h_{\kappa}^s - h_{i-1}^{n+1}}{h_i^{n+1} - h_{i-1}^{n+1}}$ and then

$$\int_{y_{i-1}}^{y_i} \beta(h(t^{n+1}, z)) \Phi(t^{n+1}, z) dz$$

$$\approx (y^* - y_{i-1}) \beta(h_{i-1}^{n+1}) \Phi(t^{n+1}, y_{i-1}) dy + (y_i - y^*) \beta(h_i^{n+1}) \Phi(t^{n+1}, y_i) dy$$

INTMOC-scheme (NASG)

▼ **Enthalpy** - key idea:

$$\frac{\frac{d}{d\tau} \tilde{h}_i^{n+1}(\tau)}{\beta(\tilde{h}_i^{n+1}(\tau)) \left(\tilde{h}_i^{n+1}(\tau) - \hat{q}(\tilde{h}_i^{n+1}(\tau)) \right)} = \frac{\Phi(\tau, \chi(\tau; t^{n+1}, y_i))}{p_0}$$

$$\int_{\tilde{h}_i^{n+1}(\bar{t})}^{\tilde{h}_i^{n+1}(t^{n+1})} \frac{1}{\beta(h)(h - \hat{q}(h))} dh = \frac{1}{p_0} \int_{\bar{t}}^{t^{n+1}} \Phi(\tau, \chi(\tau; t^{n+1}, y_i)) d\tau$$

so that

$$\tilde{h}_i^{n+1}(t^{n+1}) = R^{-1} \left(R(\tilde{h}_i^{n+1}(\bar{t})) + \frac{1}{p_0} \int_{\bar{t}}^{t^{n+1}} \Phi(\tau, \chi(\tau; t^{n+1}, y_i)) d\tau \right)$$

where

$$R(h) \stackrel{\text{def}}{=} \int_0^{\tilde{h}} \frac{1}{\beta(h)(h - \hat{q}(h))} dh$$

INTMOC-scheme (NASG)

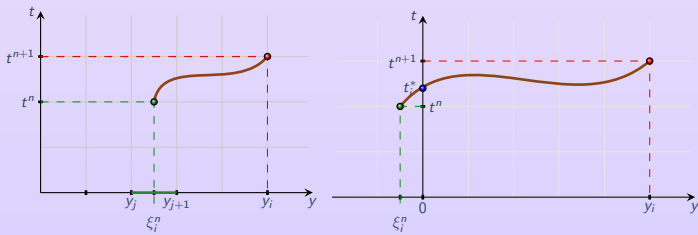
▼ **Enthalpy** - scheme: let $\xi_i^n \approx \chi(t^n; t^{n+1}, y_i)$.

- If $\xi_i^n > 0$, let $\hat{h}_i^n \approx \tilde{h}_i^{n+1}(t^n)$ (at order 1 or 2) and then $\bar{t} = t^n$ and

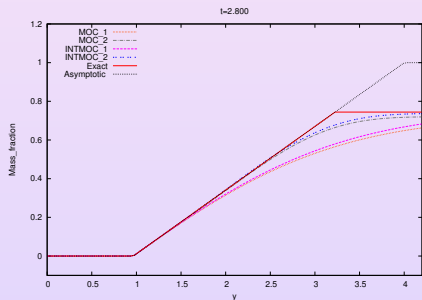
$$h_i^{n+1} = R^{-1} \left(R(\hat{h}_i^n) + \frac{\Delta t}{\rho_0} \frac{\Phi(t^n, \xi_i^n) + \Phi(t^{n+1}, y_j)}{2} \right)$$

- If $\xi_i^n \leq 0$, let $t_i^* = t^{n+1} - y_i/v_i^n \approx \tau$ such that $\chi(\tau; t^{n+1}, y_i) = 0$ and then $\bar{t} = t_i^*$ and

$$h_i^{n+1} = R^{-1} \left(R(h_e(t_i^*)) + \frac{t^{n+1} - t_i^*}{\rho_0} \frac{\Phi(t_i^*, 0) + \Phi(t^{n+1}, y_i)}{2} \right)$$

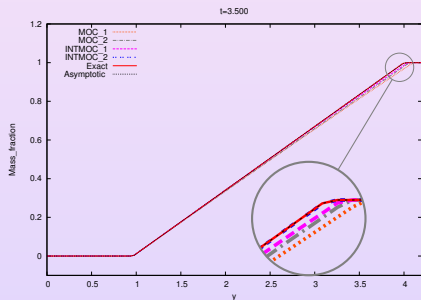
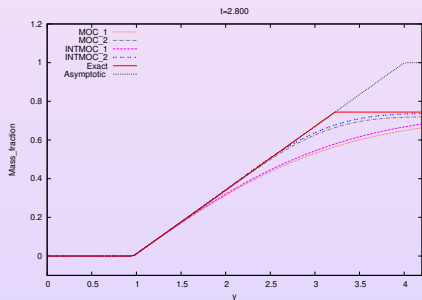


SG: MOC (order 1 or 2) vs INTMOC (order 1 or 2)



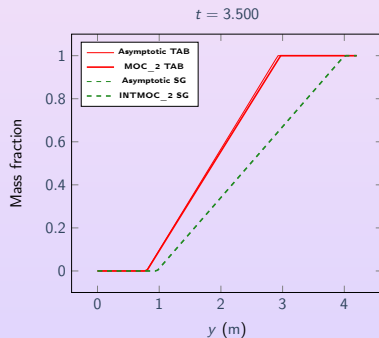
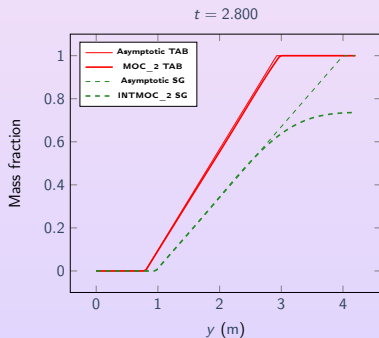
- Initially the domain is filled with liquid phase
- At $t = 1.769$ s mixture appears for $y > y_\ell^s \simeq 0.964$ m
- At $t = 2.929$ s pure vapor phase appears for $y > y_g^s \simeq 4.002$ m
- The asymptotic state is reached at $t = 2.957$ s

SG: MOC (order 1 or 2) vs INTMOC (order 1 or 2)

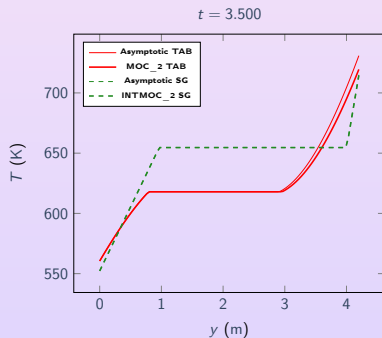
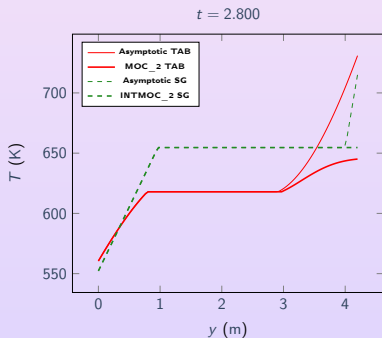


- Initially the domain is filled with liquid phase
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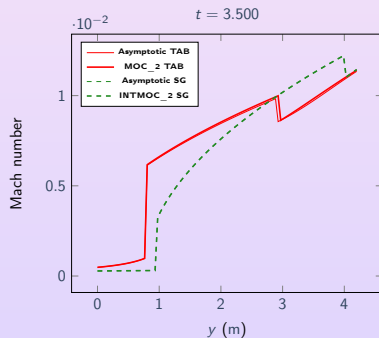
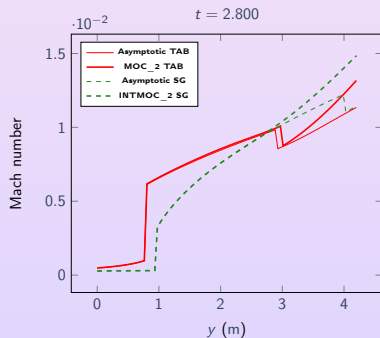
SG (INTMOC 2) vs TAB (MOC 2)



SG (INTMOC 2) vs TAB (MOC 2)

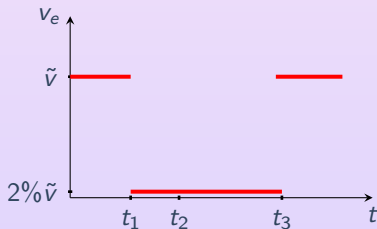


SG (INTMOC 2) vs TAB (MOC 2)

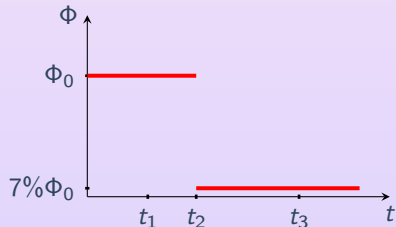


Loss of Flow Accident

$$v_e(t) = \begin{cases} \tilde{v} & \text{if } 0 \leq t < t_1, \\ 2\% \tilde{v} & \text{if } t_1 \leq t < t_3, \\ \tilde{v} & \text{if } t \geq t_3, \end{cases}$$



$$\Phi(t) = \begin{cases} \Phi_0 & \text{if } 0 \leq t < t_2, \\ 7\% \Phi_0 & \text{if } t \geq t_2. \end{cases}$$



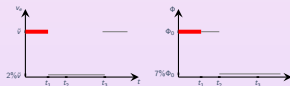
Coolant pump trip event

- pumps are stopped when $t = t_1$
- and re-started when $t = t_3$

Emergency stop

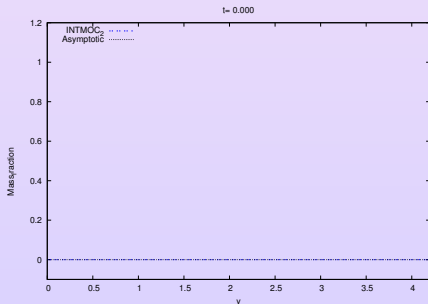
Control rods drop into the core when $t = t_2$

Loss of Flow Accident

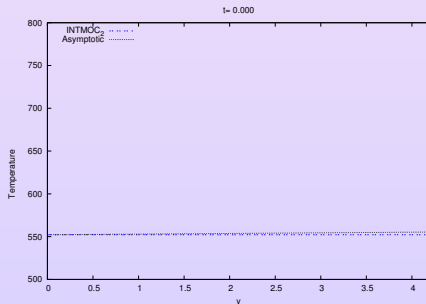


Initial data: $v_e(t) = \tilde{v}$ and $\Phi(t, y) = \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

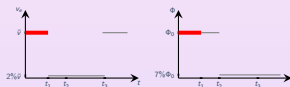
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

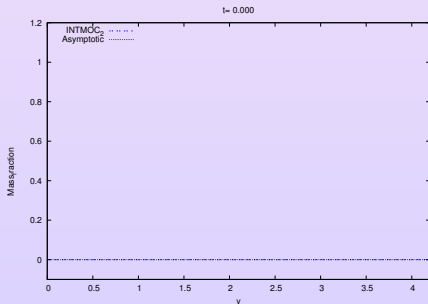
▶▶▶ Fin

Loss of Flow Accident

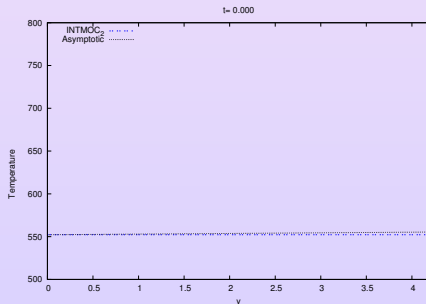


Initial data: $v_e(t) = \tilde{v}$ and $\Phi(t, y) = \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ [t₀ - t₁]

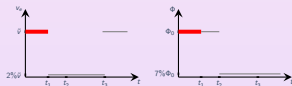
▶ [t₁ - t₂]

▶▶ [t₂ - t₃]

▶▶▶ t > t₃

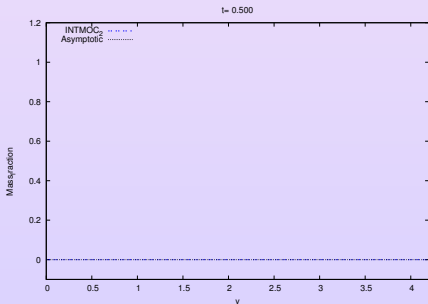
▶▶▶ Fin

Loss of Flow Accident

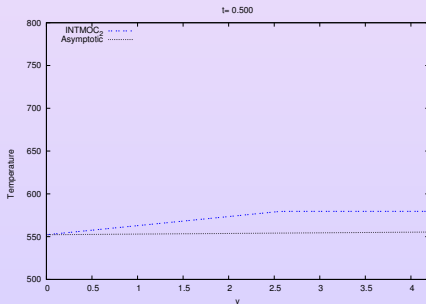


Initial data: $v_e(t) = \tilde{v}$ and $\Phi(t, y) = \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

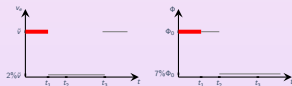
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

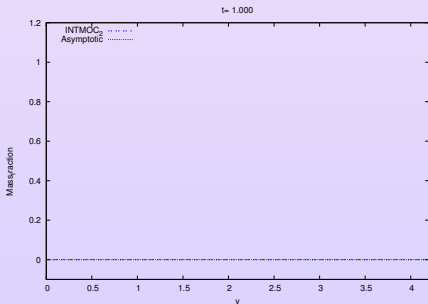
▶▶▶ Fin

Loss of Flow Accident

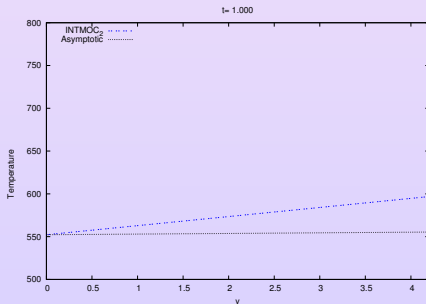


Initial data: $v_e(t) = \tilde{v}$ and $\Phi(t, y) = \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

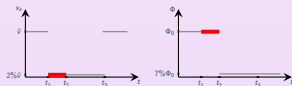
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

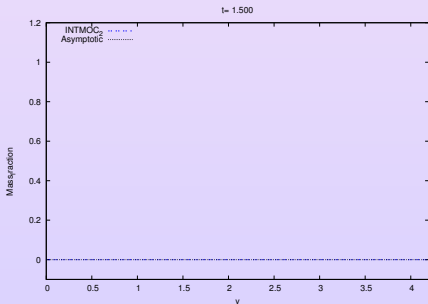
▶▶▶ Fin

Loss of Flow Accident

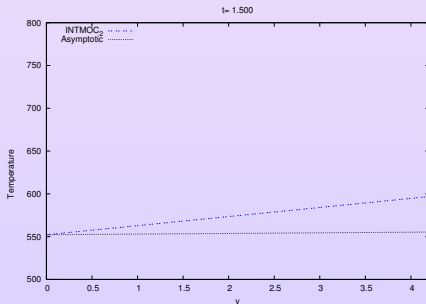


At t_1 most of the pumps stop $\implies v_e(t) \searrow$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

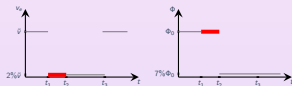
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

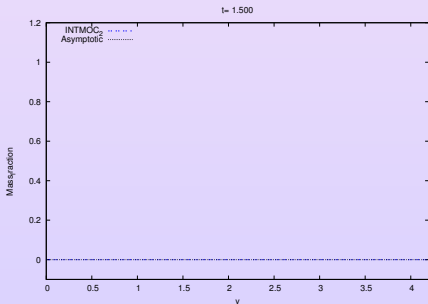
▶▶▶ Fin

Loss of Flow Accident

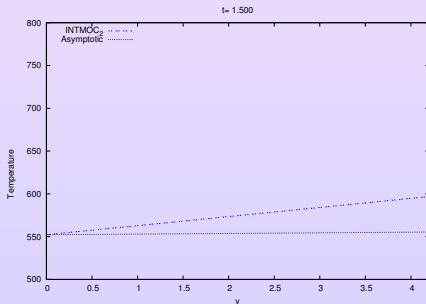


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

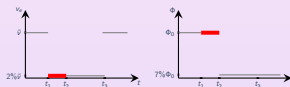
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

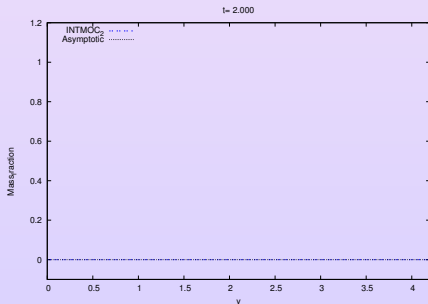
▶▶▶ Fin

Loss of Flow Accident

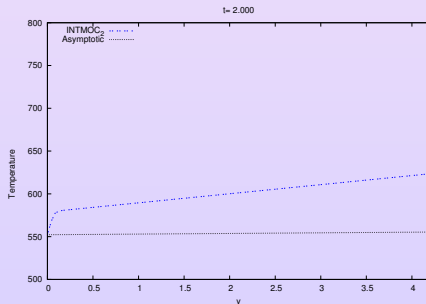


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

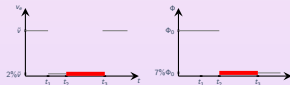
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

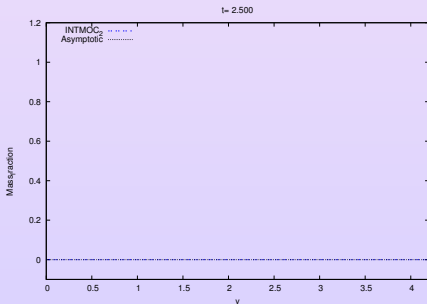
▶▶▶ Fin

Loss of Flow Accident

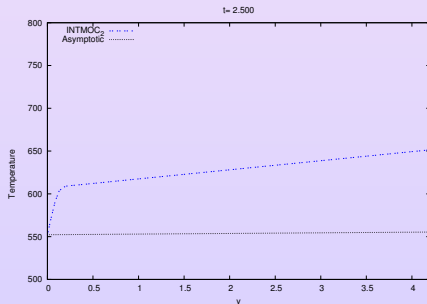


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

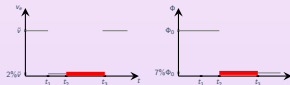
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

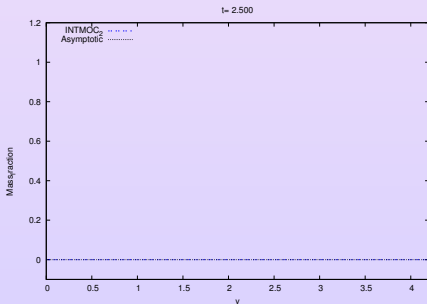
▶▶▶ Fin

Loss of Flow Accident

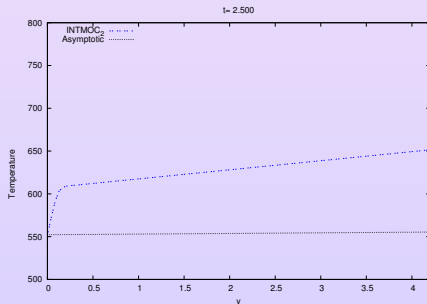


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

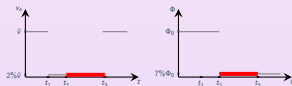
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

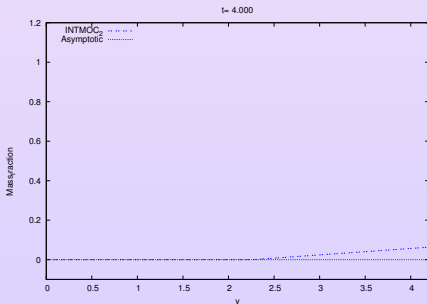
▶▶▶ Fin

Loss of Flow Accident

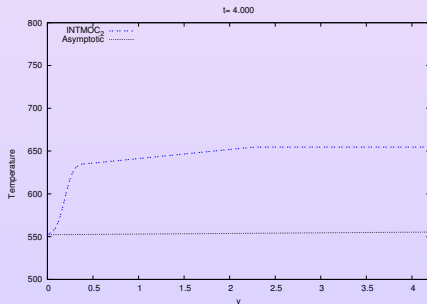


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

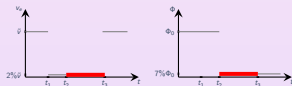
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

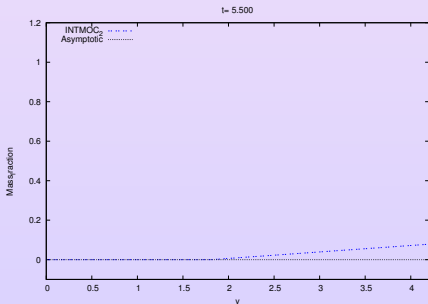
▶▶▶ Fin

Loss of Flow Accident

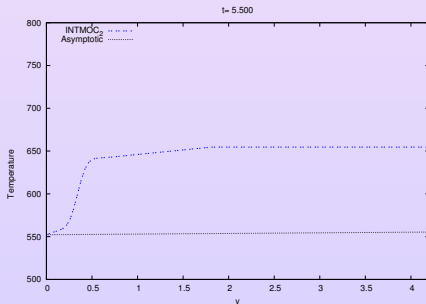


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

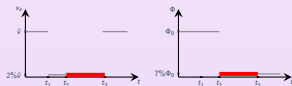
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

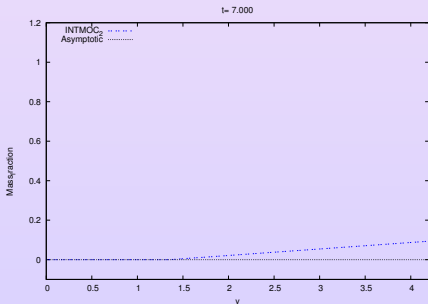
▶▶▶ Fin

Loss of Flow Accident

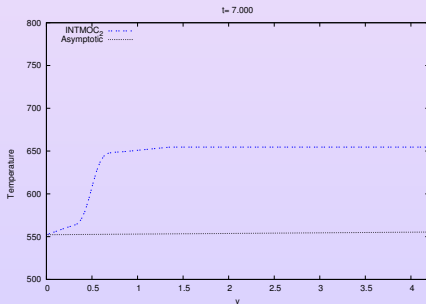


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

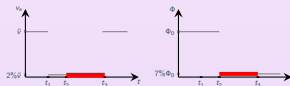
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

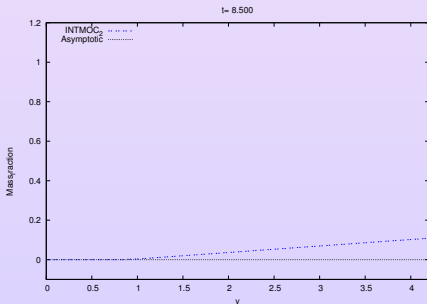
▶▶▶ Fin

Loss of Flow Accident

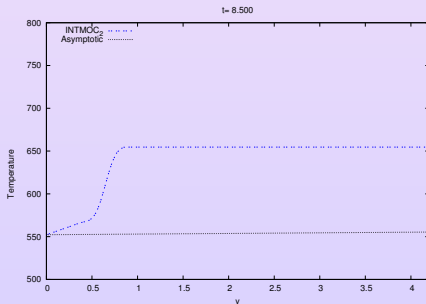


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

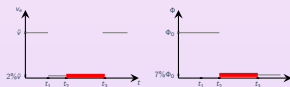
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

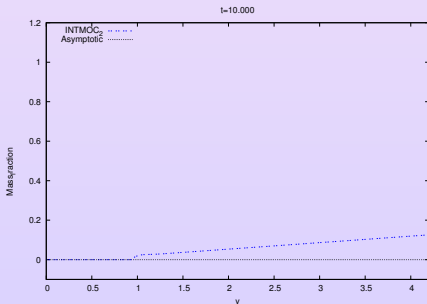
▶▶▶ Fin

Loss of Flow Accident

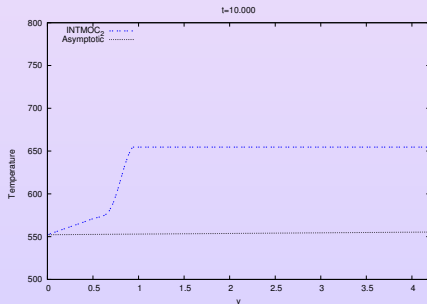


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

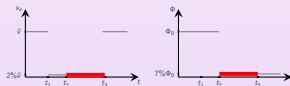
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

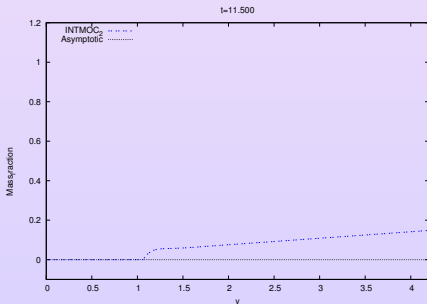
▶▶▶ Fin

Loss of Flow Accident

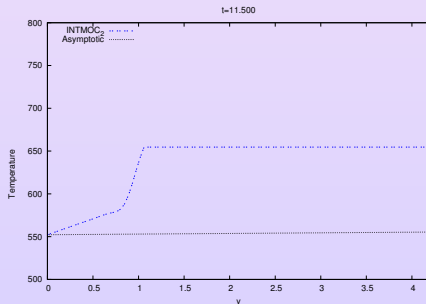


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

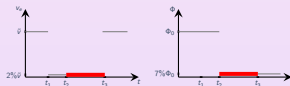
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

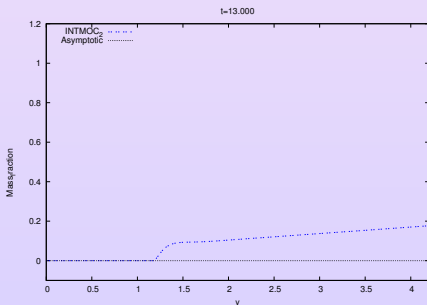
▶▶▶ Fin

Loss of Flow Accident

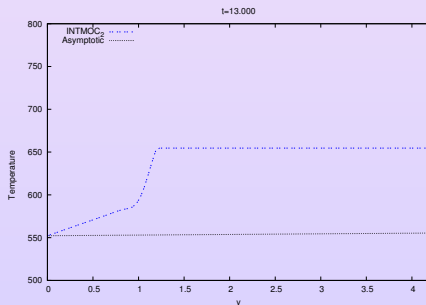


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

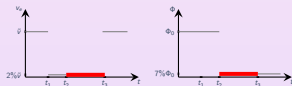
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

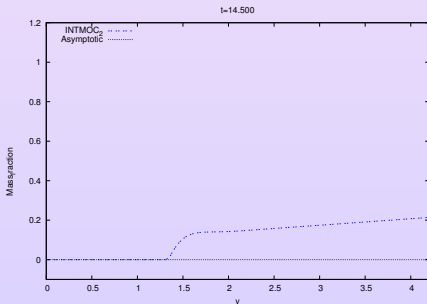
▶▶▶ Fin

Loss of Flow Accident

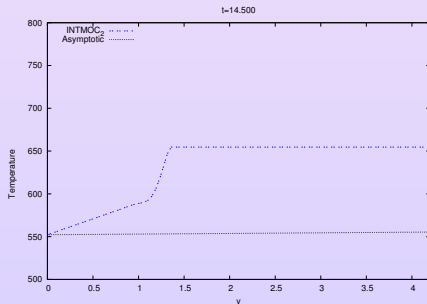


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

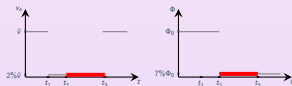
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

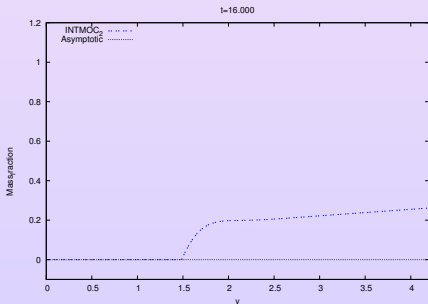
▶▶▶ Fin

Loss of Flow Accident

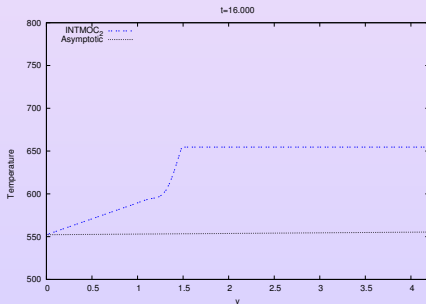


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

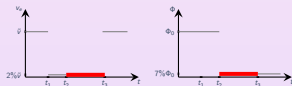
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

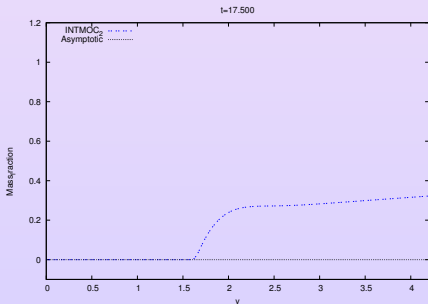
▶▶▶ Fin

Loss of Flow Accident

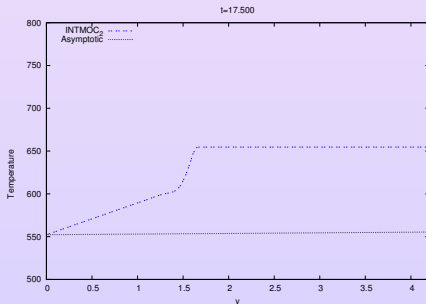


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

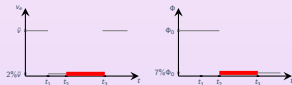
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

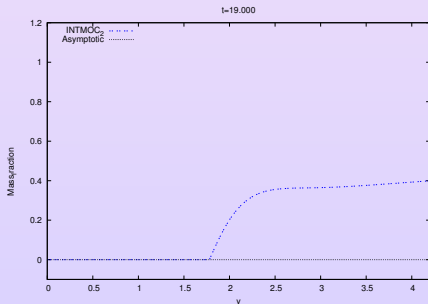
▶▶▶ Fin

Loss of Flow Accident

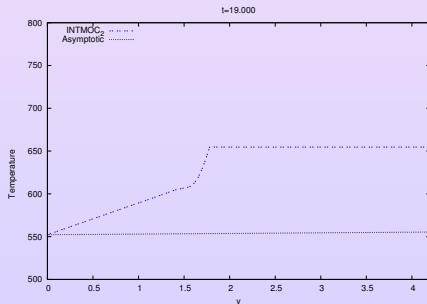


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

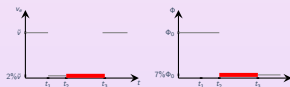
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

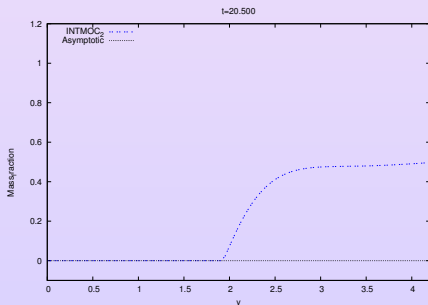
▶▶▶ Fin

Loss of Flow Accident

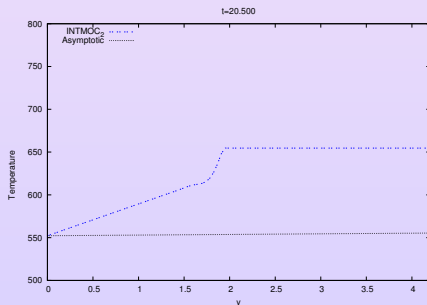


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

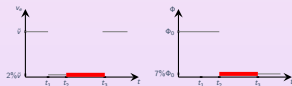
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

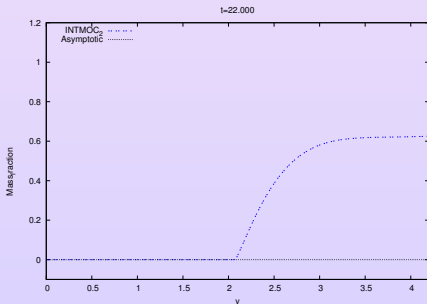
▶▶▶ Fin

Loss of Flow Accident

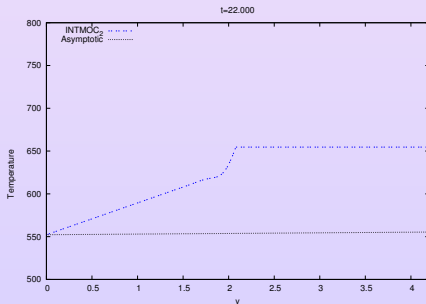


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

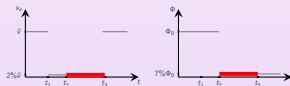
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

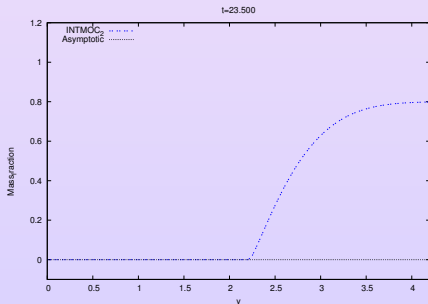
▶▶▶ Fin

Loss of Flow Accident

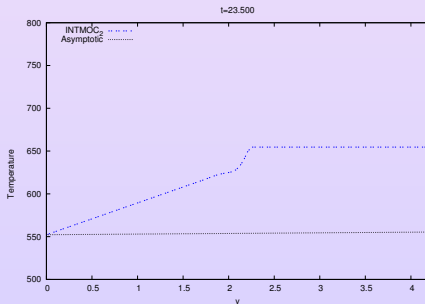


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

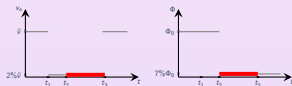
Mass fraction



Temperature

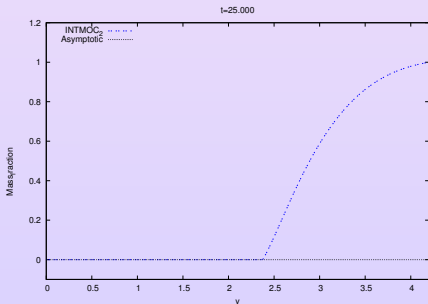

[◀ Description](#)
[▶ \[t₀ - t₁\]](#)
[▶ \[t₁ - t₂\]](#)
[▶▶ \[t₂ - t₃\]](#)
[▶▶▶ t > t₃](#)
[▶▶▶ Fin](#)

Loss of Flow Accident

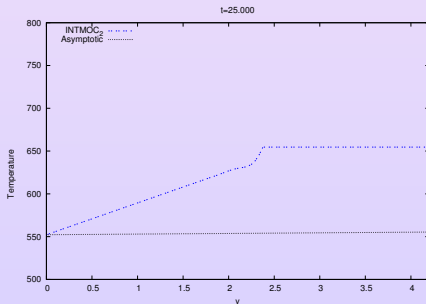


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

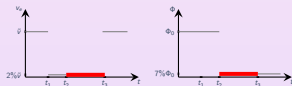
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

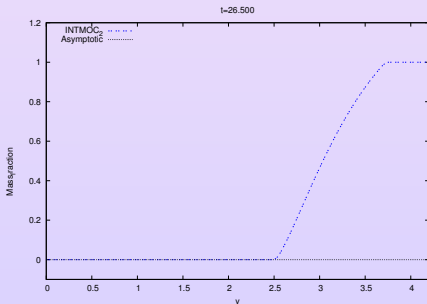
▶▶▶ Fin

Loss of Flow Accident

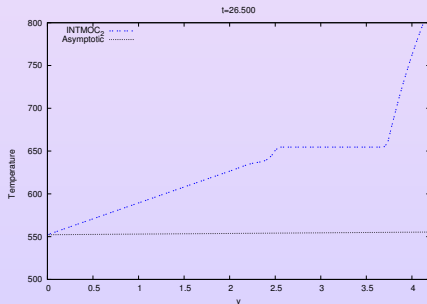


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

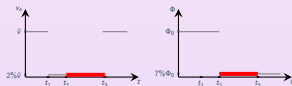
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

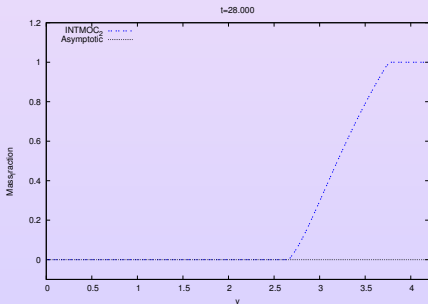
▶▶▶ Fin

Loss of Flow Accident

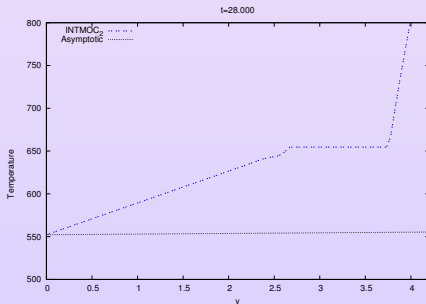


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

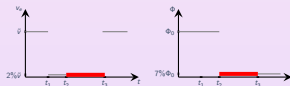
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

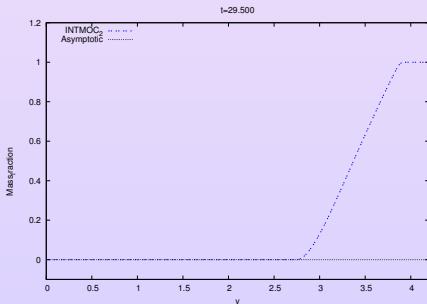
▶▶▶ Fin

Loss of Flow Accident

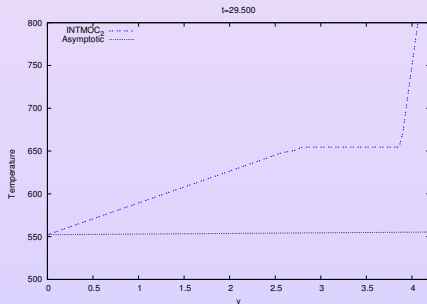


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Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

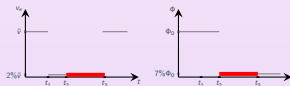
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

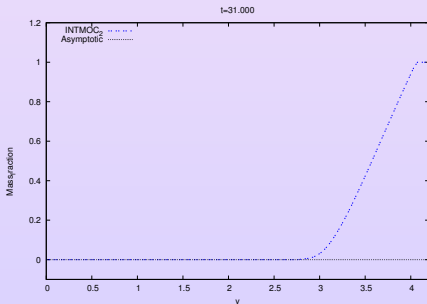
▶▶▶ Fin

Loss of Flow Accident

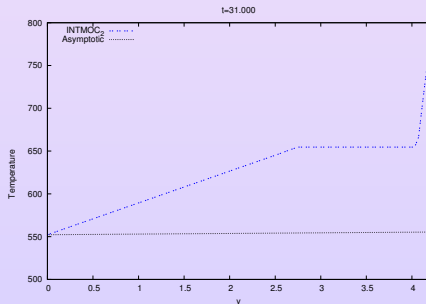


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

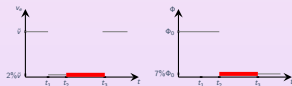
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

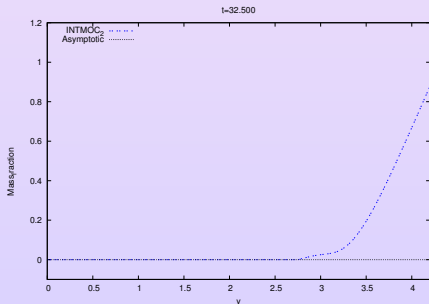
▶▶▶ Fin

Loss of Flow Accident

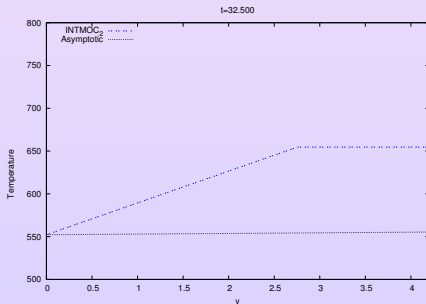


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

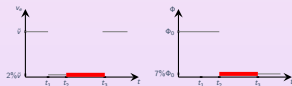
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

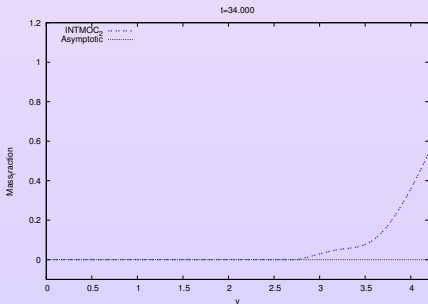
▶▶▶ Fin

Loss of Flow Accident

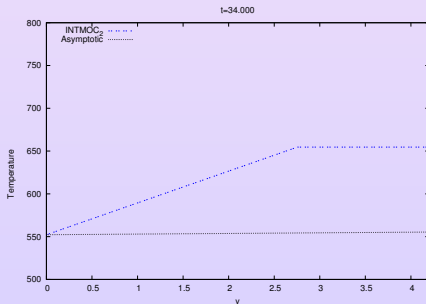


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

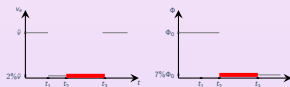
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

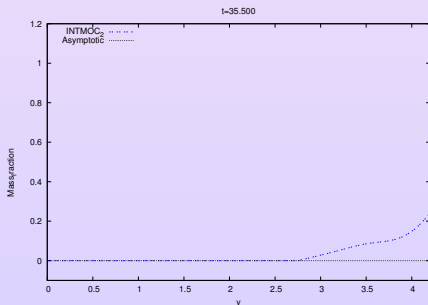
▶▶▶ Fin

Loss of Flow Accident

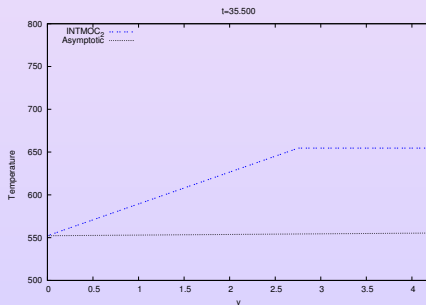


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

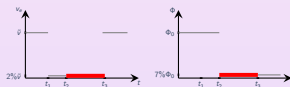
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

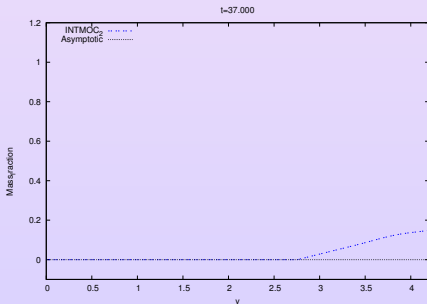
▶▶▶ Fin

Loss of Flow Accident

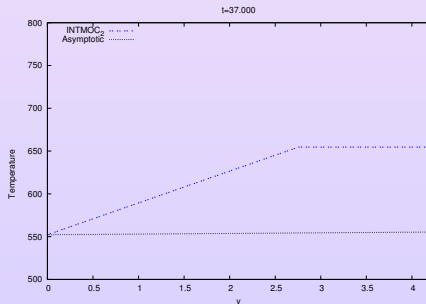


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

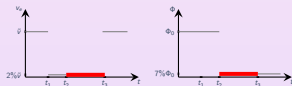
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

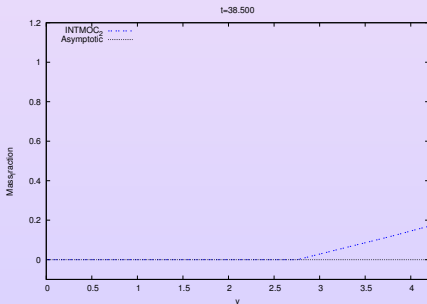
▶▶▶ Fin

Loss of Flow Accident

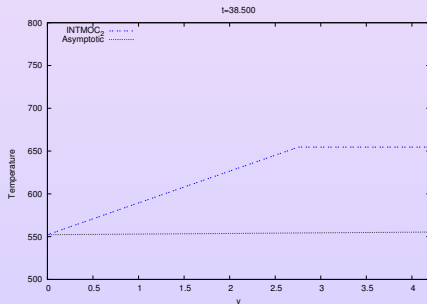


At t_2 the security system drops control rods into the core $\implies \Phi(t) \searrow 7\% \Phi_0$.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

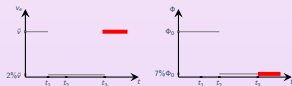
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

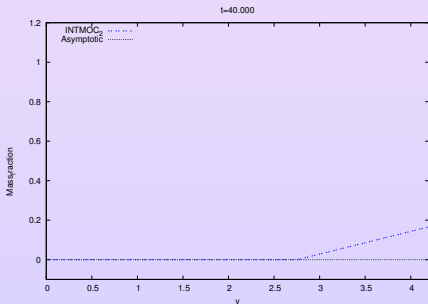
▶▶▶ Fin

Loss of Flow Accident

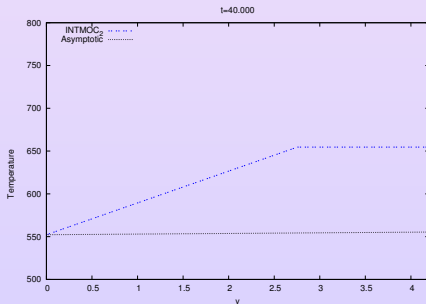


At t_3 the security pumps are turned on $\implies v_e(t) \nearrow$ and the fluid comes back to the liquid phase.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

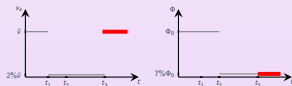
▶ $[t_1 - t_2]$

▶▶ $[t_2 - t_3]$

▶▶▶ $t > t_3$

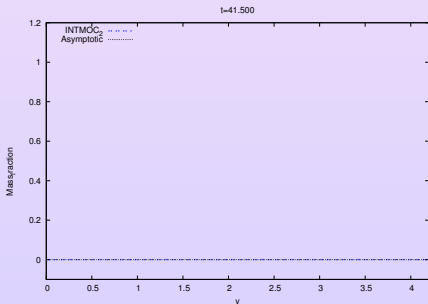
▶▶▶ Fin

Loss of Flow Accident

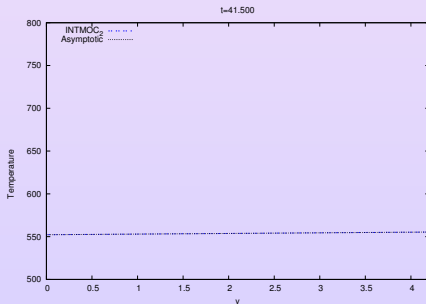


At t_3 the security pumps are turned on $\implies v_e(t) \nearrow$ and the fluid comes back to the liquid phase.

Mass fraction



Temperature



◀ Description

▶ $[t_0 - t_1]$

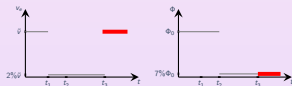
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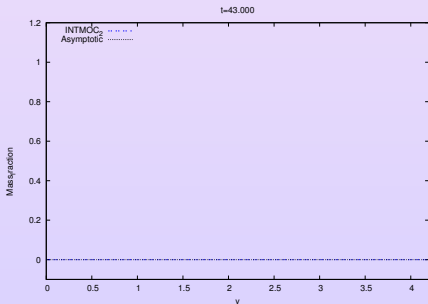
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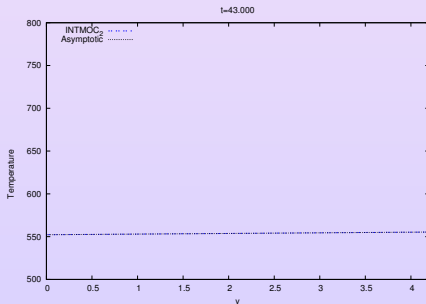


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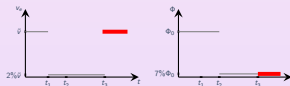
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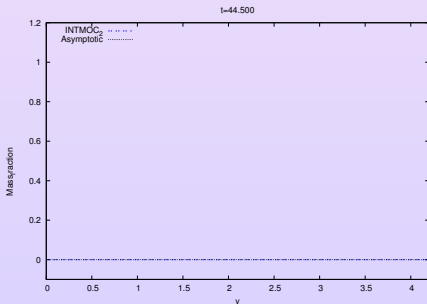
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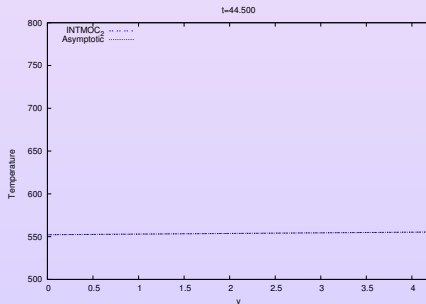


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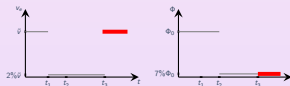
Mass fraction



Temperature

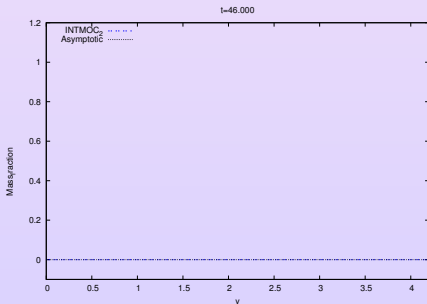

[◀ Description](#)
[▶ \[t₀ - t₁\]](#)
[▶ \[t₁ - t₂\]](#)
[▶▶ \[t₂ - t₃\]](#)
[▶▶▶ t > t₃](#)
[▶▶▶ Fin](#)

Loss of Flow Accident

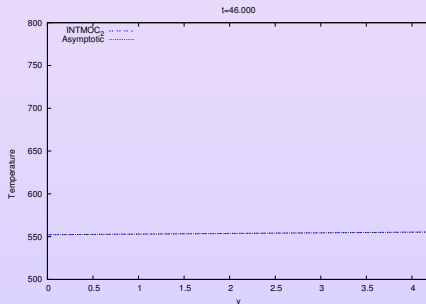


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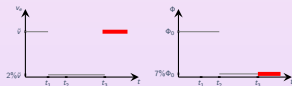
Mass fraction



Temperature

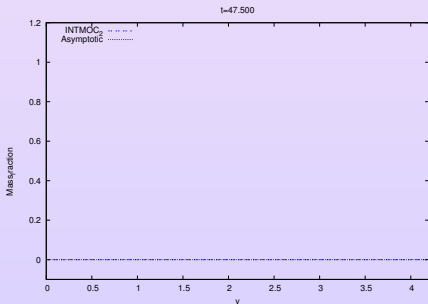

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Loss of Flow Accident

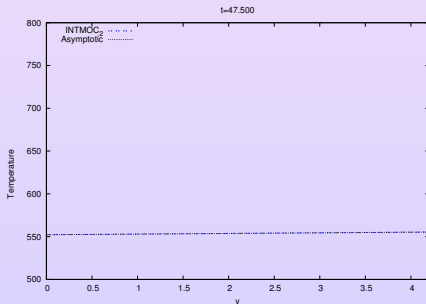


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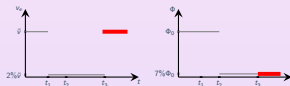
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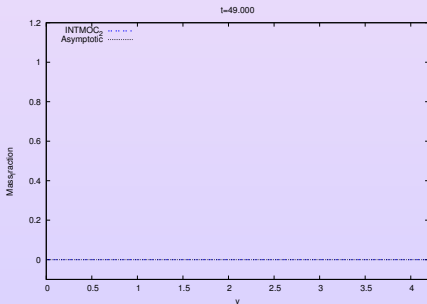
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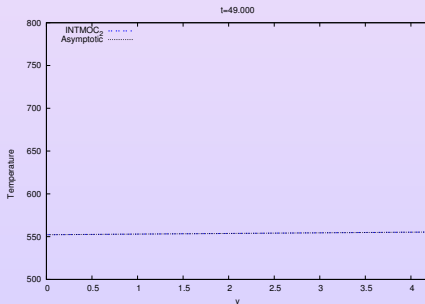


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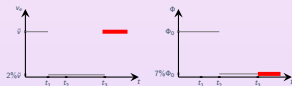
Mass fraction



Temperature

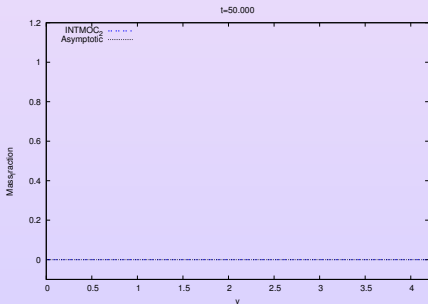

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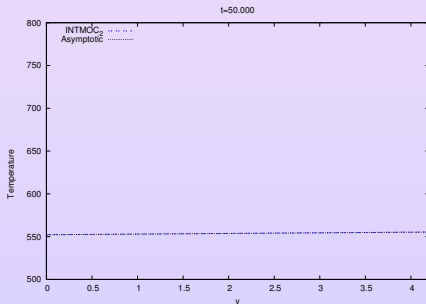


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▶ $[t_0 - t_1]$

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▶▶▶ $t > t_3$

▶▶▶ Fin

Section 5

Numerical schemes

- 1D Numerical schemes
- 2D Numerical scheme

FreeFem++ (1)

- Let ξ^n the foot at time t^n of the characteristic issuing from \mathbf{x} at time t^{n+1} , then the convective part of the system can be approximated by

$$[\partial_t \star + (\mathbf{u} \cdot \nabla) \star](t^{n+1}, \mathbf{x}) \approx \frac{\star(t^{n+1}, \mathbf{x}) - \star(t^n, \xi^n)}{\Delta t}, \quad \star = \mathbf{u} \text{ or } h$$

- Weak formulation of a semi-implicit temporal discretization: at time t^{n+1} find $(\mathbf{u}^{n+1}, \bar{p}^{n+1}, h^{n+1}) \in (\mathbf{u}_e + \mathcal{U}) \times \mathcal{P} \times (h_e + \mathcal{H})$ defined by

- $\mathcal{U} = \{\mathbf{v} \in (H^1(\Omega))^2 \mid \mathbf{v}(x, 0) = \mathbf{0}, \mathbf{v} \cdot \mathbf{n}(0, y) = \mathbf{v} \cdot \mathbf{n}(L_x, y) = 0\}$
- $\mathcal{P} = L_0^2(\Omega) = \{q \in L^2(\Omega) \mid \int_{\Omega} q(\mathbf{x}) \, d\mathbf{x} = 0\}$
- $\mathcal{H} = \{k \in H^1(\Omega) \mid k(x, 0) = 0\}$

such that ...

FreeFem++ (2)

- $\forall \mathbf{u}_{\text{test}} \in \mathcal{U}$

$$\begin{aligned} & \frac{1}{\Delta t} \int_{\Omega} \varrho(h^n)(\mathbf{u}^{n+1} - \mathbf{u}^n(\xi^n)) \cdot \mathbf{u}_{\text{test}} \, d\mathbf{x} \\ & + \int_{\Omega} \mu(h^n)((\nabla \mathbf{u}^{n+1} + (\nabla \mathbf{u}^{n+1})^T) : \nabla(\mathbf{u}_{\text{test}})) \, d\mathbf{x} \\ & + \int_{\Omega} \eta(h^n) \operatorname{div}(\mathbf{u}^{n+1}) \operatorname{div}(\mathbf{u}_{\text{test}}) \, d\mathbf{x} - \int_{\Omega} \bar{p}^{n+1} \operatorname{div}(\mathbf{u}_{\text{test}}) \, d\mathbf{x} \\ & = \int_{\Omega} \varrho(h^n) \mathbf{g} \cdot \mathbf{u}_{\text{test}} \, d\mathbf{x} \end{aligned}$$

- $\forall p_{\text{test}} \in \mathcal{P}$

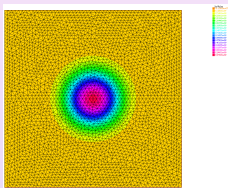
$$\int_{\Omega} \operatorname{div}(\mathbf{u}^{n+1}) p_{\text{test}} \, d\mathbf{x} = \frac{1}{p_0} \int_{\Omega} \beta(h^n) \Phi(t^{n+1}) p_{\text{test}} \, d\mathbf{x}$$

- $\forall h_{\text{test}} \in \mathcal{H}$

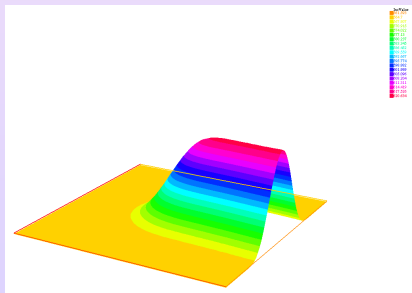
$$\frac{1}{\Delta t} \int_{\Omega} (h^{n+1} - h^n(\xi^n)) h_{\text{test}} \, d\mathbf{x} = \int_{\Omega} \frac{\Phi(t^{n+1})}{\varrho(h^n)} h_{\text{test}} \, d\mathbf{x}$$

A 2D test

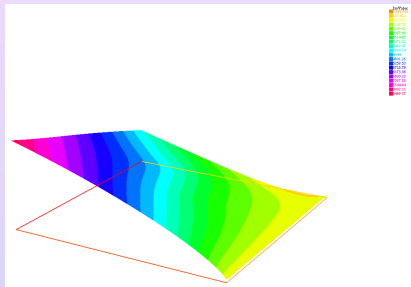
- Power density localized in the center of the core
- Gravity along $(1, -1)$



Power density and mesh



Temperature

Pressure $(\bar{p} - \min_{\Omega} \bar{p})$

Section 6

Conclusion & Perspectives

Summary & Perspectives

- Model

- ✓ mono/diphasic low Mach model with phase transition (Noble Able Stiffened Gas & Tabulated EoS),
- ✓ $t \mapsto p_0(t)$,
- ✓ Heat diffusion,

- Theoretical study (1D)

- ✓ unsteady exact solutions on some cases (NASG with phase transition),
steady exact solutions (also with tabulated EOS),

- Numerical Method

- ✓ preliminary results: 1D (MOC, unconditionally positive)& 2D (MOC+FE)

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- ✗ Coupling with a neutronics model
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- Numerical Method

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- ✗ 3D (FV with projection, C. Galusinski, J.-M. Maurizi).

Appendix

- ▶ References
- ▶ Compressible Navier-Stokes system
- ▶ Computing saturation values from two pure phase laws
- ▶ $p \rightarrow T^s$
- ▶ NIST vs SG
- ▶ Tabulated laws
- ▶ MOC

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-  S. Dellacherie.
On a low Mach nuclear core model.
ESAIM Proc., 35:79–106, 2012.
-  M. Bernard, S. Dellacherie, G. Faccanoni, B. Grec, O. Lafitte, T.-T. Nguyen and Y. Penel.
Study of low Mach nuclear core model for single-phase flow.
ESAIM Proc., 38:118–134, 2012.
-  M. Bernard, S. Dellacherie, G. Faccanoni, B. Grec and Y. Penel.
Study of low Mach nuclear core model for two-phase flows with phase transition I: stiffened gas law.
Submitted.
-  S. Dellacherie, G. Faccanoni, B. Grec, E. Nayir and Y. Penel.
2D numerical simulation of a low Mach nuclear core model with stiffened gas using FreeFem++
Submitted
-  S. Dellacherie, G. Faccanoni, B. Grec and Y. Penel.
Study of a low Mach model for two-phase flows with phase transition II: tabulated laws.
In preparation.

Compressible Navier-Stokes system

$$\begin{cases} \partial_t \varrho + \operatorname{div}(\varrho \mathbf{u}) = 0 \\ \partial_t(\varrho \mathbf{u}) + \operatorname{div}(\varrho \mathbf{u} \otimes \mathbf{u}) = -\nabla p + \operatorname{div}(\sigma(\mathbf{u})) + \varrho \mathbf{g} \\ \partial_t(\varrho h) + \operatorname{div}(\varrho h \mathbf{u}) = \partial_t p + \mathbf{u} \cdot \nabla p + \sigma(\mathbf{u}) : \nabla \mathbf{u} + \Phi \end{cases}$$

where

$$\sigma(\mathbf{u}) \stackrel{\text{def}}{=} \nu(\nabla \mathbf{u} + (\nabla \mathbf{u})^T) + \eta \nabla \mathbf{u}$$

- ▶ **Unknowns**
- ▶ **Given quantities**
- ▶ **Equation Of State**

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where

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▼ Unknowns

- $(t, \mathbf{x}) \mapsto \mathbf{u}$ velocity,
- $(t, \mathbf{x}) \mapsto h$ enthalpy,
- $(t, \mathbf{x}) \mapsto p$ pressure;

▶ Given quantities

▶ Equation Of State

Compressible Navier-Stokes system

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► **Unknowns**

▼ **Given quantities**

- $(t, x) \mapsto \Phi \geq 0$ power density,
- \mathbf{g} gravity;

► **Equation Of State**

Compressible Navier-Stokes system

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► **Unknowns**

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▼ **Equation Of State**

- $(h, p) \mapsto \nu, \eta$ such that $2\mu + 3\eta > 0$,
- $(h, p) \mapsto \varrho$ density.

Saturation values

- Liquid $\kappa = \ell$ and vapor $\kappa = g$ are characterized by their EoS

$$(h, p) \mapsto \varrho_{\kappa} = \frac{\gamma_{\kappa}}{\gamma_{\kappa} - 1} \frac{p + \pi_{\kappa}}{h - q_{\kappa}}$$

(see [Le Metayer and Saurel](#) for parameters of liquid water and steam)

- Second principle of thermodynamics: when phases coexist, they have the same pressures, the same temperatures and their chemical potentials are equal:

$$g_{\ell}(p, T) = g_g(p, T) \quad \implies \quad T = T^s(p).$$

- We define saturation values at $p = p_0$:

$$h_{\kappa}^s \stackrel{\text{def}}{=} h_{\kappa}(p_0, T^s(p_0)), \quad \varrho_{\kappa}^s \stackrel{\text{def}}{=} \varrho_{\kappa}(h_{\kappa}^s, p_0).$$

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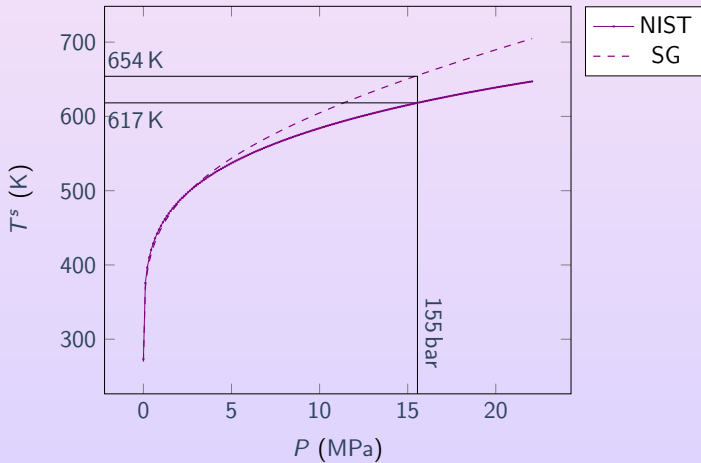
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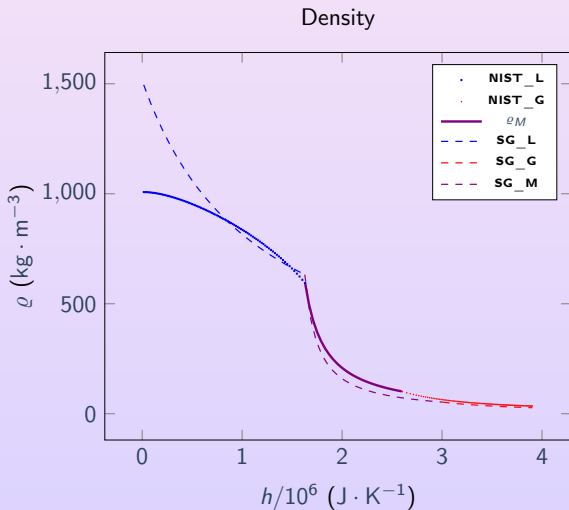
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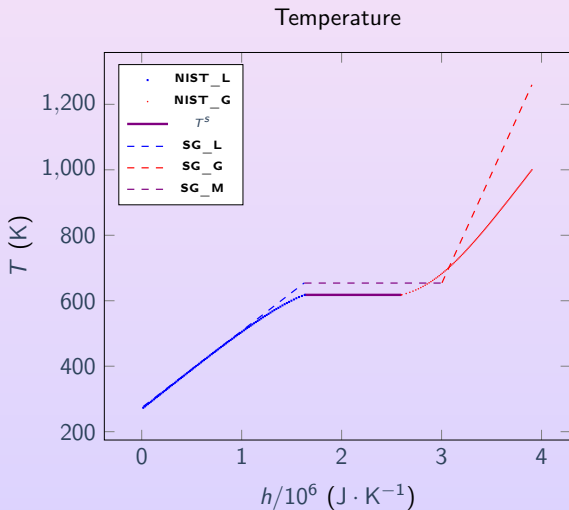
$$p \mapsto T^s$$



NIST vs SG

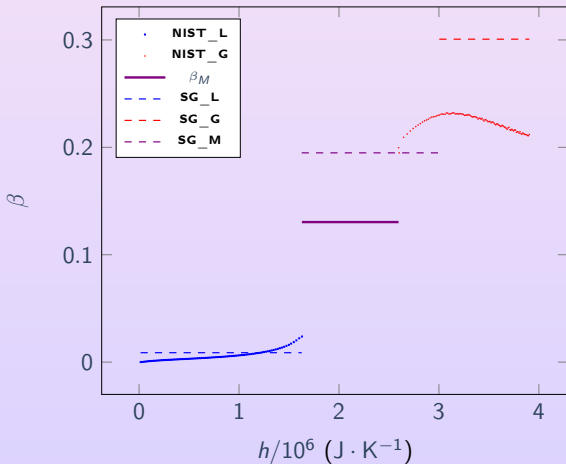
	NIST	SG
T^s	617 K	654 K
h_ℓ^s	$1.629 \times 10^6 \text{ J} \cdot \text{K}^{-1}$	$1.627 \times 10^6 \text{ J} \cdot \text{K}^{-1}$
h_g^s	$2.596 \times 10^6 \text{ J} \cdot \text{K}^{-1}$	$3.004 \times 10^6 \text{ J} \cdot \text{K}^{-1}$
ρ_ℓ^s	$594.38 \text{ kg} \cdot \text{m}^{-3}$	$632.663 \text{ kg} \cdot \text{m}^{-3}$
ρ_g^s	$101.93 \text{ kg} \cdot \text{m}^{-3}$	$52.937 \text{ kg} \cdot \text{m}^{-3}$

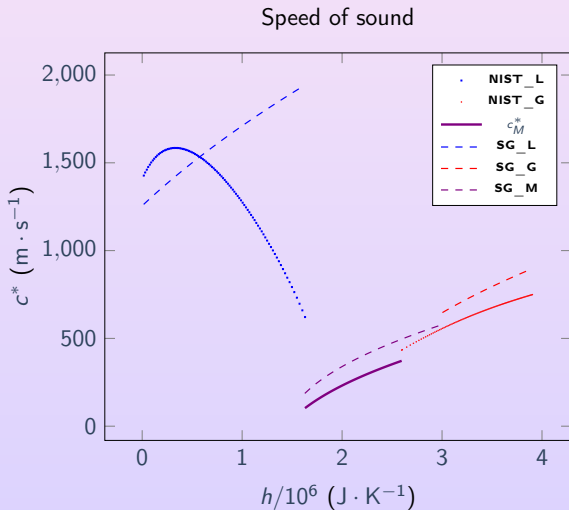
NIST vs SG: $h \mapsto \rho$ 

NIST vs SG: $h \mapsto T$ 

NIST vs SG: $h \mapsto \beta$

Compressibility coefficient



NIST vs SG: $h \mapsto c^*$ 

Pure phase EoS: Tabulated laws at $p = p_0$

κ	h [kJ/kg]	ρ_κ [kg/m ³]	T_κ [K]	c_κ^* [m · s ⁻¹]	β_κ
l	15.608	1007.5	273.16	1427.4	X
l	30.678	1007.5	276.79	1445.0	X
\vdots	\vdots	\vdots	\vdots	\vdots	\vdots
l	1602.8	609.10	614.77	659.56	X
l	h_ℓ^s	594.38	T^s	621.43	X
g	h_g^s	101.93	T^s	433.40	X
g	2602.6	101.06	618.41	435.61	X
\vdots	\vdots	\vdots	\vdots	\vdots	\vdots
g	2.5299	35.139	996.37	747.83	X
g	2.5290	34.985	1000.0	749.37	X

Source: <http://webbook.nist.gov/chemistry/fluid/>

Pure phase EoS: Tabulated laws at $p = p_0$

Liquid phase

- Discretization of the enthalpy interval $[1.56 \times 10^4; h_\ell^s]$:

$$h_i \simeq (1.56 + 1.68i) \times 10^4, \quad i \in \mathcal{I} = \{1, \dots, 96\}$$

- Approximation of $\beta_\ell(h_i) = -\frac{p_0}{\varrho_\ell^2(h_i)} \varrho'_\ell(h_i)$ by finite differences
- Least squares polynomial approximation over the set of discrete values $((\varrho_\ell, \beta_\ell, T_\ell, c_\ell^*)(h_i))_{i \in \mathcal{I}}$:

$$(\varrho_\ell, \beta_\ell, T_\ell, c_\ell^*) \left(\frac{h}{10^6} \right) = \sum_{j=0}^N \left(\frac{h}{10^6} \right)^j a_j, \quad N \leq 6$$

Pure phase EoS: Tabulated laws at $p = p_0$

Vapor phase

- Discretization of the enthalpy interval $[h_g^s; 25.29 \times 10^6]$:

$$h_i \simeq (2.596 + 0.0122i) \times 10^6, \quad i \in \mathcal{I} = \{1, \dots, 107\}$$

- Approximation of $\beta_g(h_i) = -\frac{p_0}{\varrho_g^2(h_i)} \varrho'_g(h_i)$ by finite differences
- Least squares polynomial approximation over the set of discrete values $((\varrho_g, \beta_g, T_g, c_g^*)(h_i))_{i \in \mathcal{I}}$:

$$(\varrho_g, \beta_g, T_g, c_g^*) \left(\frac{h}{10^6} \right) = \sum_{j=0}^N \left(\frac{h}{10^6} \right)^j a_j, \quad N \leq 6$$

MOC scheme details

- 1 Foot of the characteristic $\xi_i^n \approx \chi(t^n; t^{n+1}, y_i)$.
- 2 $\hat{h}_i^n \approx h(t^n, \xi_i^n) \approx \tilde{h}_i^{n+1}(t^n)$.

MOC scheme details

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This approximation is computed either at order one or two:

- 1 at order one in time we have $\xi(t^n, y_i) \approx y_i - \Delta t \cdot v(t^n, y_i)$ so that we set

$$\xi_i^n = y_i - \Delta t \cdot v_i^n,$$

- 2 at order two in time we have

$$\xi(t^n, y_i) \approx y_i - \Delta t \cdot v(t^n, y_i) - \frac{1}{2} \Delta t^2 \left(\partial_t v(t^n, y_i) - \frac{\beta(h(t^n, y_i))}{\rho_0} v(t^n, y_i) \Phi(t^n, y_i) \right)$$

so that we set

$$\xi_i^n = y_i - \Delta t \left(\frac{3}{2} v_i^n - \frac{1}{2} v_i^{n-1} \right) + \frac{\Delta t^2}{2} \frac{\beta(h_i^n)}{\rho_0} v_i^n \Phi(t^n, y_i).$$

- 2 $\hat{h}_i^n \approx h(t^n, \xi_i^n) \approx \tilde{h}_i^{n+1}(t^n)$.

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If $\xi_i^n > 0$, let j be the index such that $\xi_i^n \in [y_j, y_{j+1})$ and $\theta_{ij}^n \stackrel{\text{def}}{=} \frac{y_{j+1} - \xi_i^n}{\Delta x}$.

1 At order one $\hat{h}_i^n = \theta_{ij}^n h_j^n + (1 - \theta_{ij}^n) h_{j+1}^n$.

2 At order two $\hat{h}_i^n = \lambda_i^n h_j^- + (1 - \lambda_i^n) h_j^+$ where

$$\lambda_i^n \stackrel{\text{def}}{=} \begin{cases} \frac{1 + \theta_{ij}^n}{3}, & \text{if } \mathcal{P}_j^+(\theta_{ij}^n) \geq 0 \text{ and } \mathcal{P}_j^-(\theta_{ij}^n) \geq 0, \\ 0, & \text{if } \mathcal{P}_j^+(\theta_{ij}^n) \geq 0 \text{ and } \mathcal{P}_j^-(\theta_{ij}^n) < 0, \\ 1, & \text{if } \mathcal{P}_j^+(\theta_{ij}^n) < 0 \text{ and } \mathcal{P}_j^-(\theta_{ij}^n) \geq 0, \\ \theta_{ij}^n, & \text{otherwise,} \end{cases}$$

$$h_j^- \stackrel{\text{def}}{=} \begin{cases} h_j^n, & \text{if } \mathcal{P}_j^+(\theta_{ij}^n) < 0 \text{ and } \mathcal{P}_j^-(\theta_{ij}^n) < 0, \\ \frac{(\theta_{ij}^n)^2}{2} (h_{j-1}^n - 2h_j^n + h_{j+1}^n) - \frac{\theta_{ij}^n}{2} (h_{j-1}^n - 4h_j^n + 3h_{j+1}^n) + h_{j+1}^n, & \text{otherwise,} \end{cases}$$

$$h_j^+ \stackrel{\text{def}}{=} \begin{cases} h_{j+1}^n, & \text{if } \mathcal{P}_j^+(\theta_{ij}^n) < 0 \text{ and } \mathcal{P}_j^-(\theta_{ij}^n) < 0, \\ \frac{(\theta_{ij}^n)^2}{2} (h_{j+2}^n - 2h_{j+1}^n + h_j^n) - \frac{\theta_{ij}^n}{2} (h_{j+2}^n - h_j^n) + h_{j+1}^n, & \text{otherwise,} \end{cases}$$

and $\mathcal{P}_j^\pm(\theta) \stackrel{\text{def}}{=} (\theta - \delta_j^\pm)(\theta - \delta_{j+1}^\pm)$ where

$$\delta_j^- \stackrel{\text{def}}{=} \frac{2(h_{j+1}^n - h_j^n)}{h_{j-1}^n - 2h_j^n + h_{j+1}^n},$$

$$\delta_{j+1}^- \stackrel{\text{def}}{=} \frac{h_{j-1}^n - 4h_j^n + 3h_{j+1}^n}{h_{j-1}^n - 2h_j^n + h_{j+1}^n},$$

$$\delta_j^+ \stackrel{\text{def}}{=} \frac{2(h_{j+1}^n - h_j^n)}{h_j^n - 2h_{j+1}^n + h_{j+2}^n},$$

$$\delta_{j+1}^+ \stackrel{\text{def}}{=} \frac{h_{j+2}^n - h_j^n}{h_j^n - 2h_{j+1}^n + h_{j+2}^n}.$$